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Green Hydrogen Webinar Series

Technologies for supply and utilization of hydrogen

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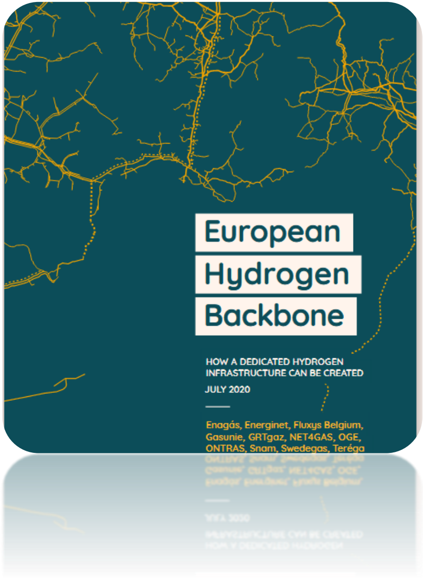
[1] [2] [3] [4] [5] [6]

Hamburg University of Technology (TUHH), Institute of Environmental Technology and Energy Economics (IUE)
www.tuhh.de/iue

Background

Compression (CGH_2)



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Liquefaction (LH_2)

[8]

Methanol (CH_3OH)

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Liquid Organic Hydrogen Carriers (LOHC)

[9]

Ammonia (NH_3)

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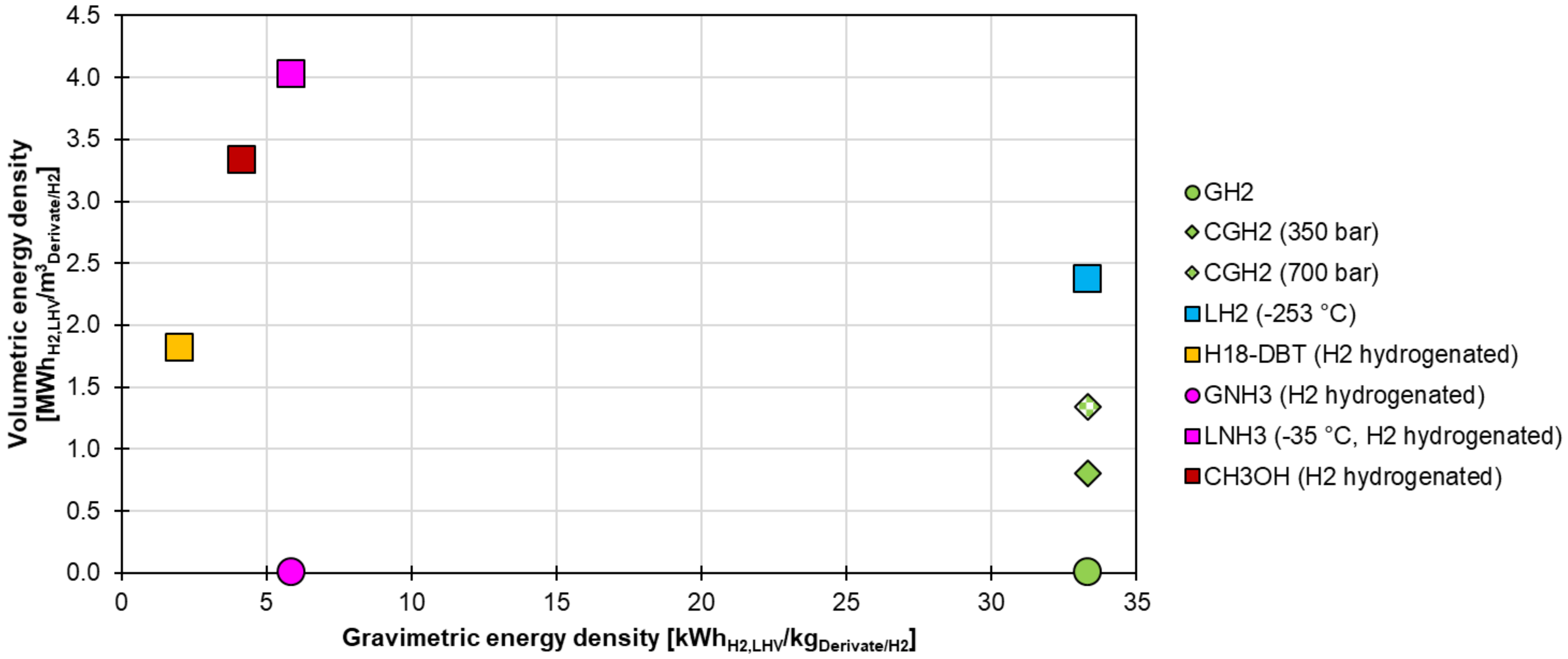
Several different conditioned hydrogen options are discussed for low cost hydrogen transportation and storage

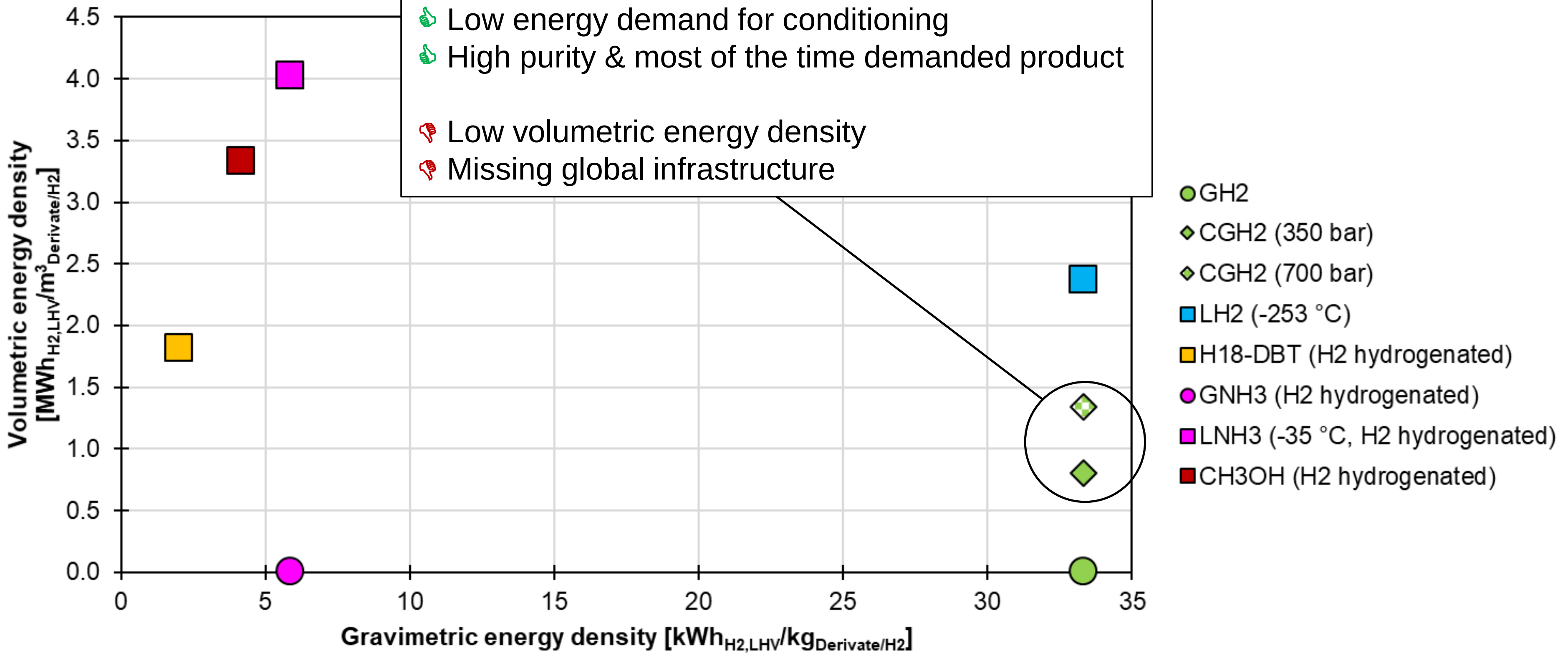
Outline

1. Conditioning Options
2. Supply Chains
3. Economic Assessment
4. Utilization

Conditioned Hydrogen Options



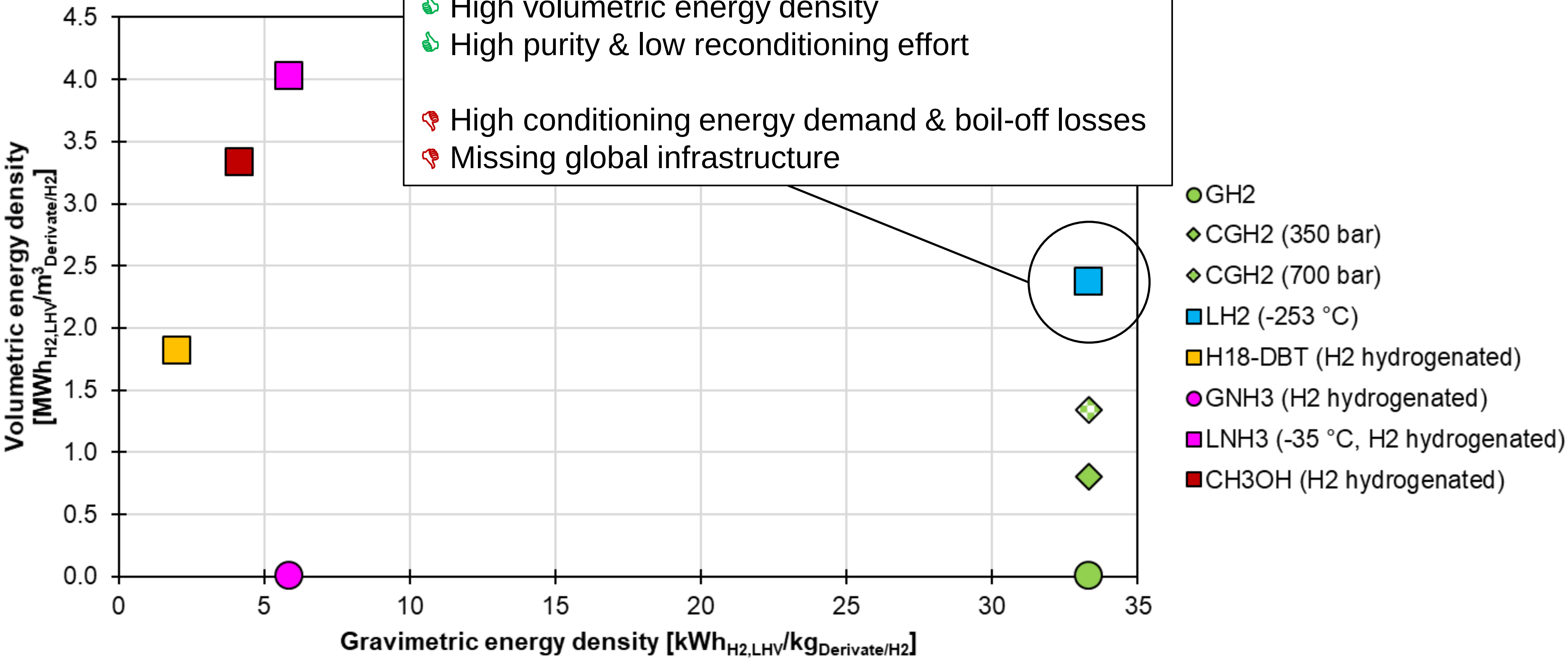
Compressed Gaseous Hydrogen (CGH_2)



- 👍 Low energy demand for conditioning
- 👍 High purity & most of the time demanded product

- 👎 Low volumetric energy density
- 👎 Missing global infrastructure

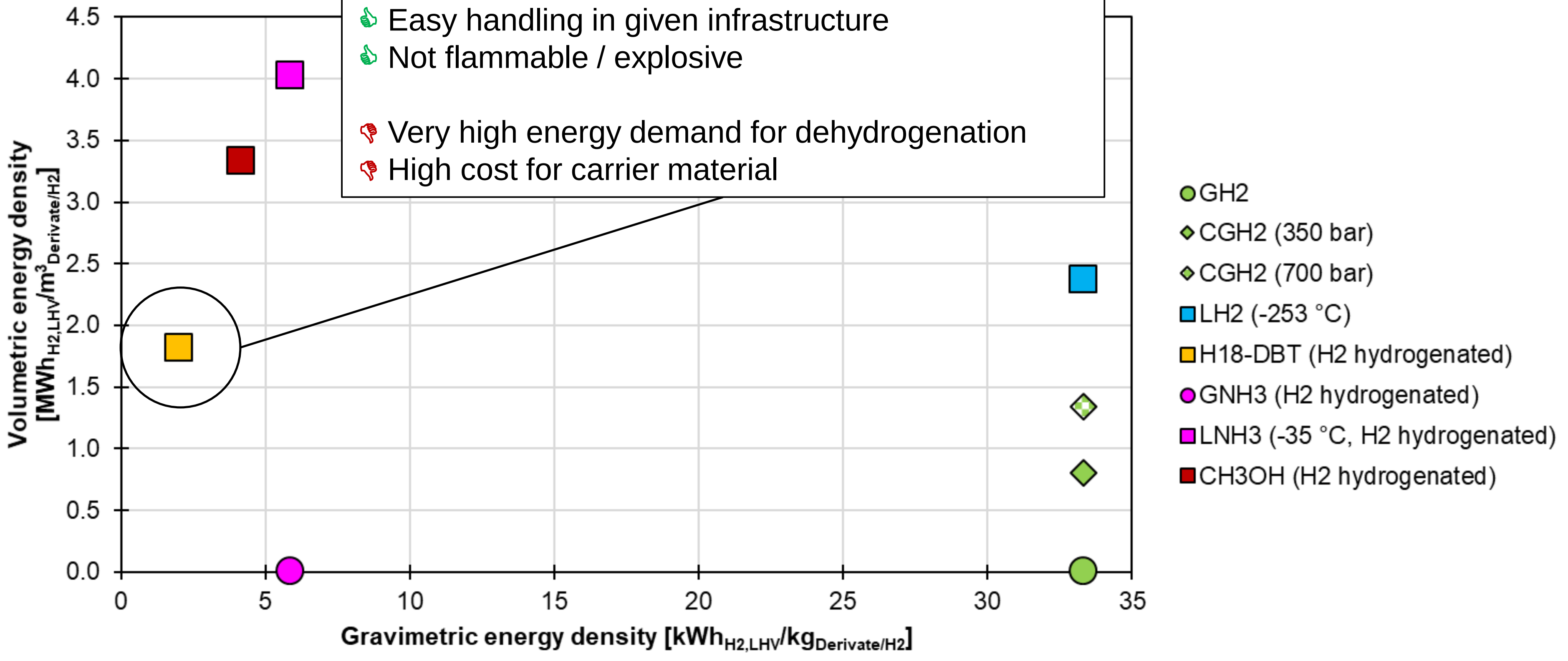
Liquid Hydrogen (LH_2)



- High volumetric energy density
- High purity & low reconditioning effort

- High conditioning energy demand & boil-off losses
- Missing global infrastructure

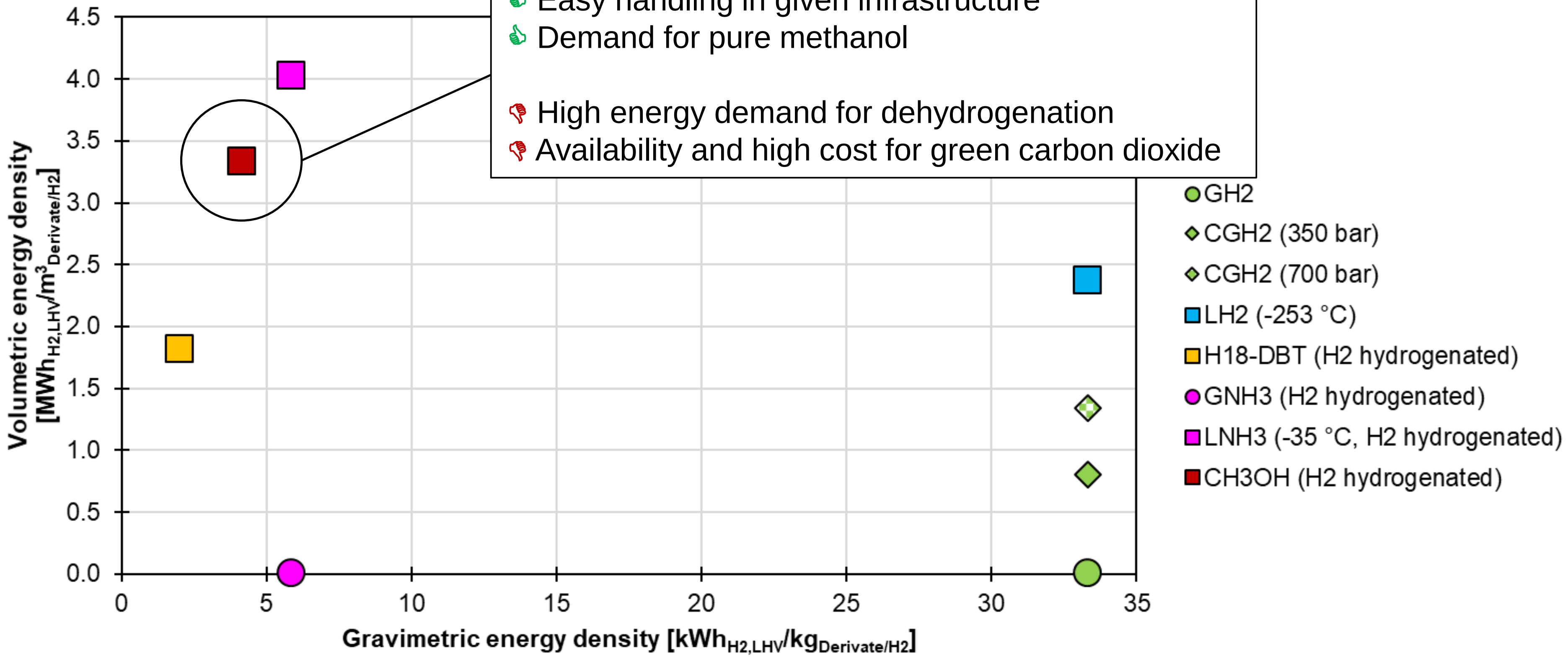
Liquid Organic Hydrogen Carrier (LOHC)



- 👍 Easy handling in given infrastructure
- 👍 Not flammable / explosive

- 👎 Very high energy demand for dehydrogenation
- 👎 High cost for carrier material

Methanol (CH_3OH)



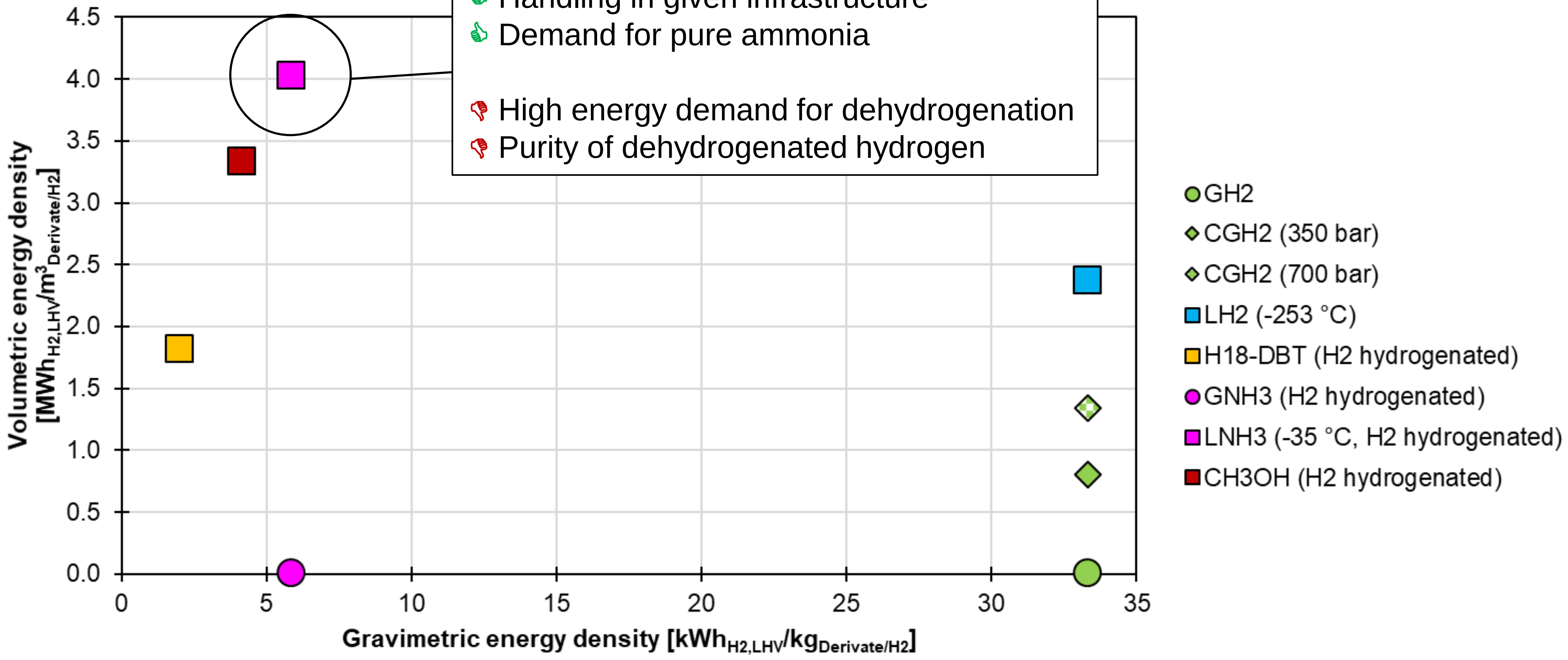
- 👍 Easy handling in given infrastructure
- 👍 Demand for pure methanol

- 👎 High energy demand for dehydrogenation
- 👎 Availability and high cost for green carbon dioxide

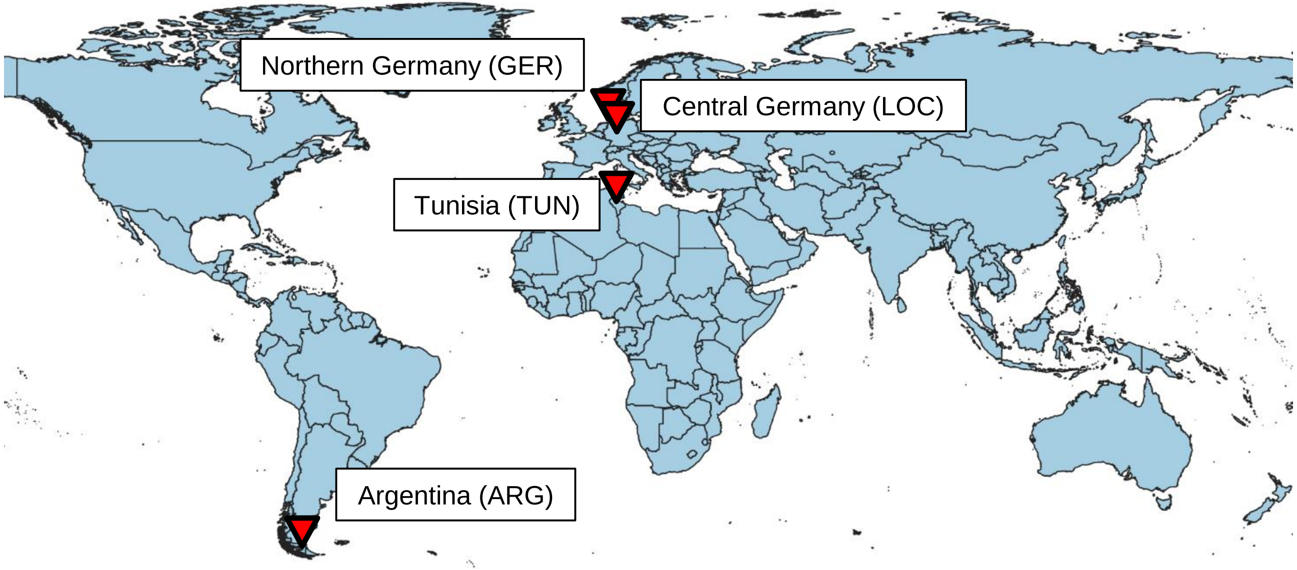
Ammonia (NH_3)

- Handling in given infrastructure
- Demand for pure ammonia

- High energy demand for dehydrogenation
- Purity of dehydrogenated hydrogen



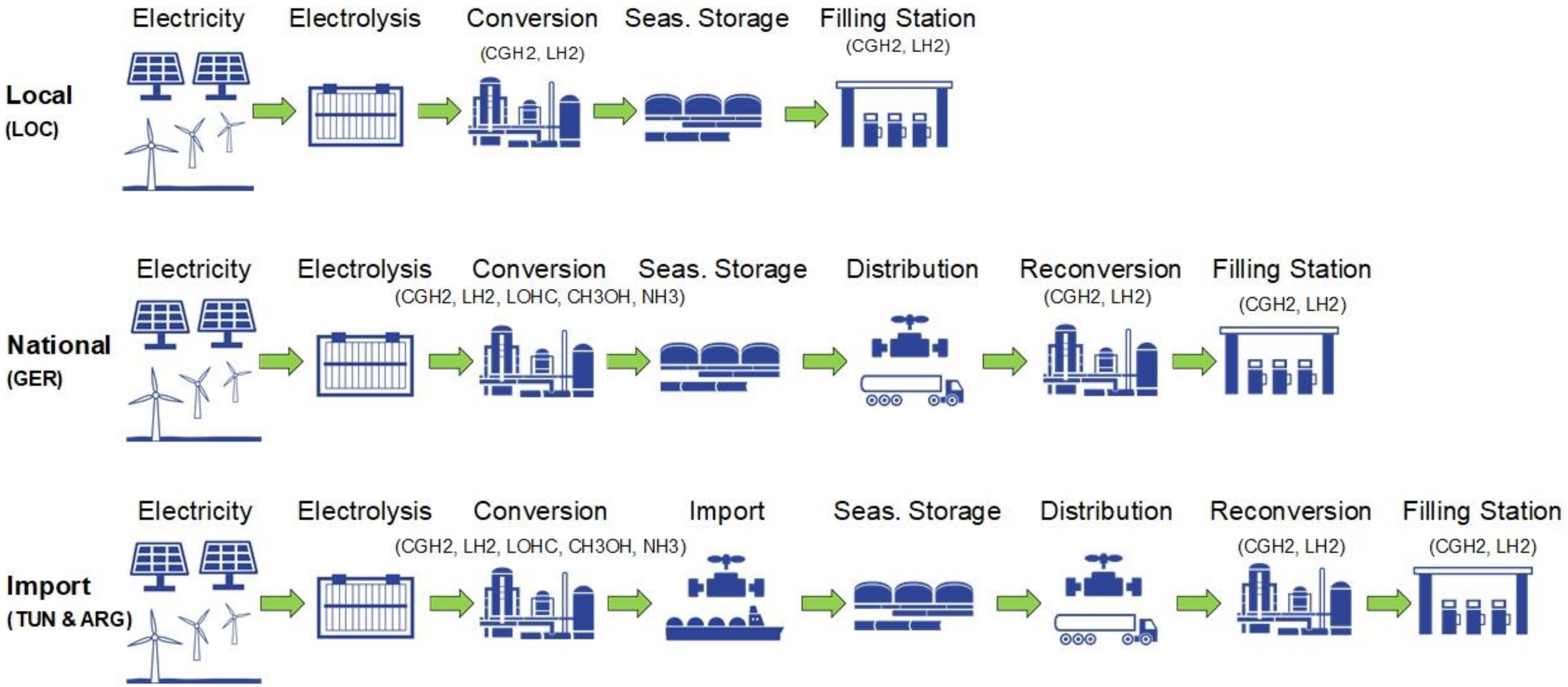
Production Locations



- **Central Germany (LOC):** PV ≈ 1,100 AFLH; Onshore Wind ≈ 2,600 AFLH
- **Northern Germany (GER):** PV ≈ 1,000 AFLH; Offshore Wind ≈ 5,000 AFLH
- **Tunisia (TUN):** PV ≈ 1,800 AFLH; Onshore Wind ≈ 3,500 AFLH
- **Argentina (ARG):** PV ≈ 1,000 AFLH; Onshore Wind ≈ 5,500 AFLH

AFLH = annual full load hours

Supply Chains



Assessment Approach

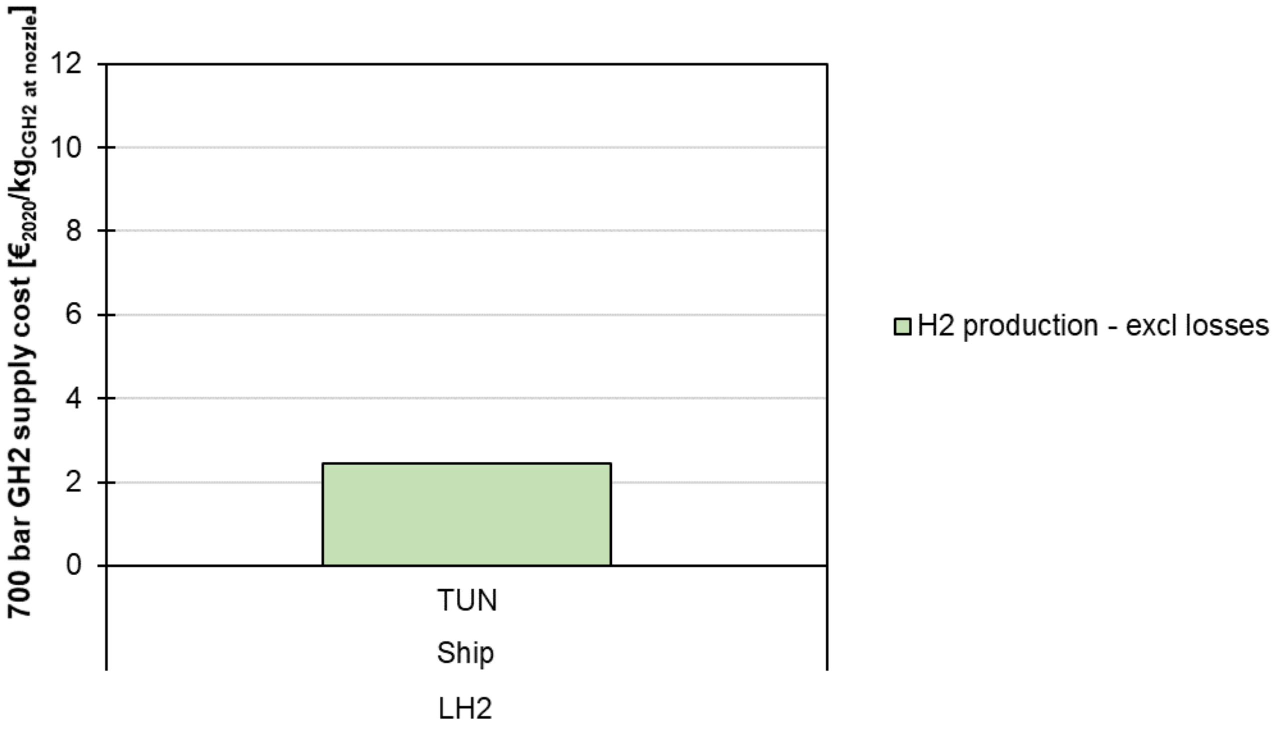
- Supply efficiency based on hydrogen (LHV) filled in tank divided by the overall chain energy input from well to tank

- Hydrogen supply cost considers the well to tank costs and is calculated with the annuity method

- Depreciation equals the technology lifetime

- Real weighted average cost of capital set to 6%

Gaseous Hydrogen Supply Cost in 2030



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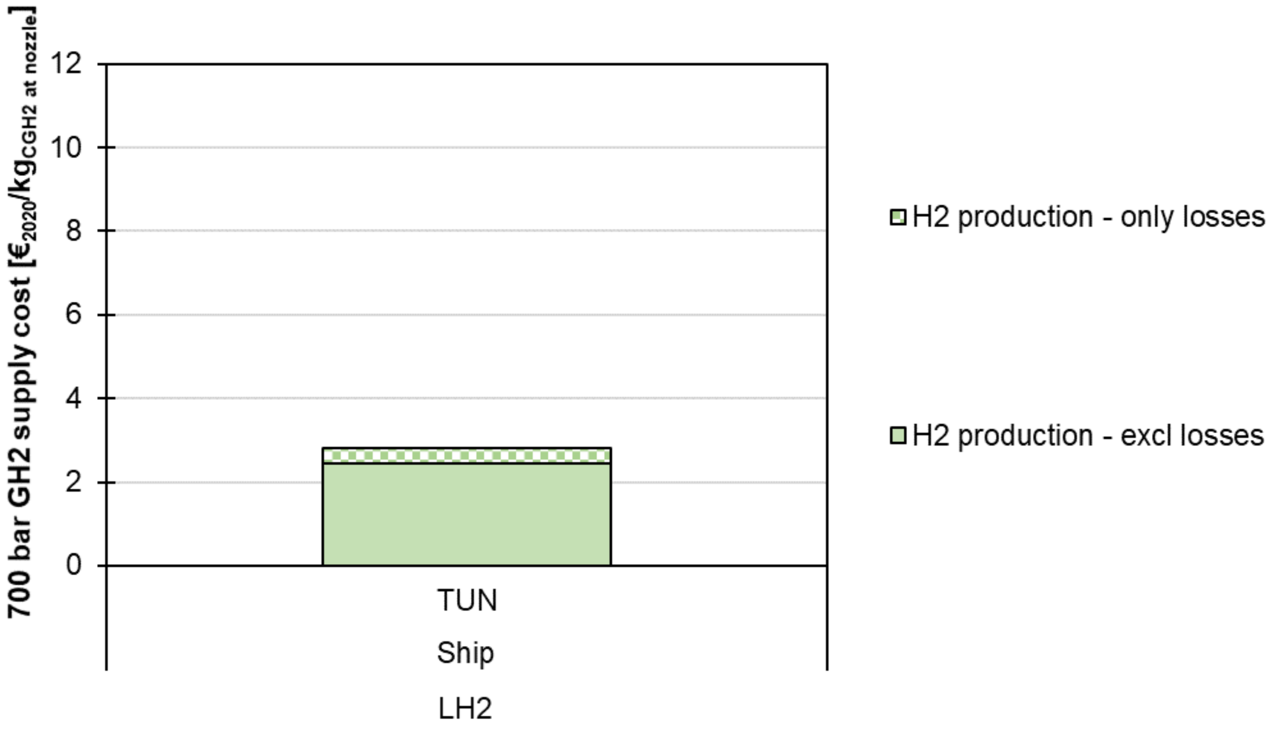

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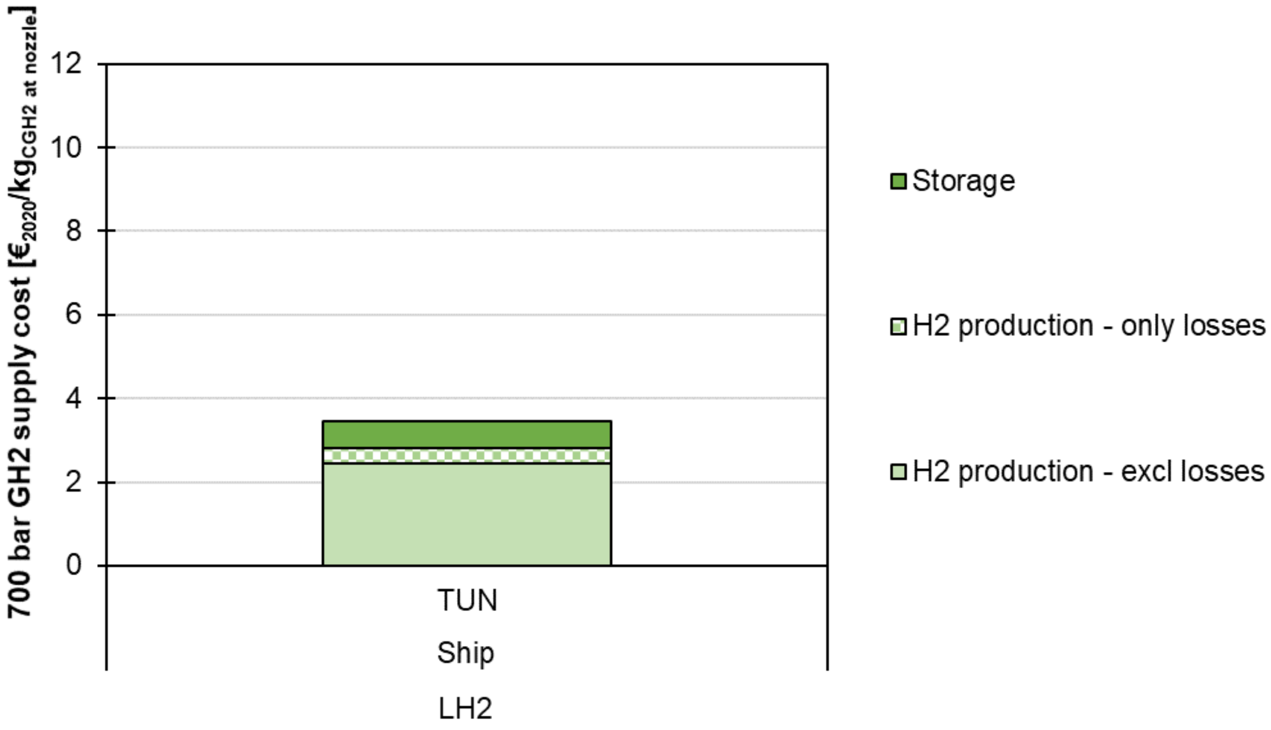

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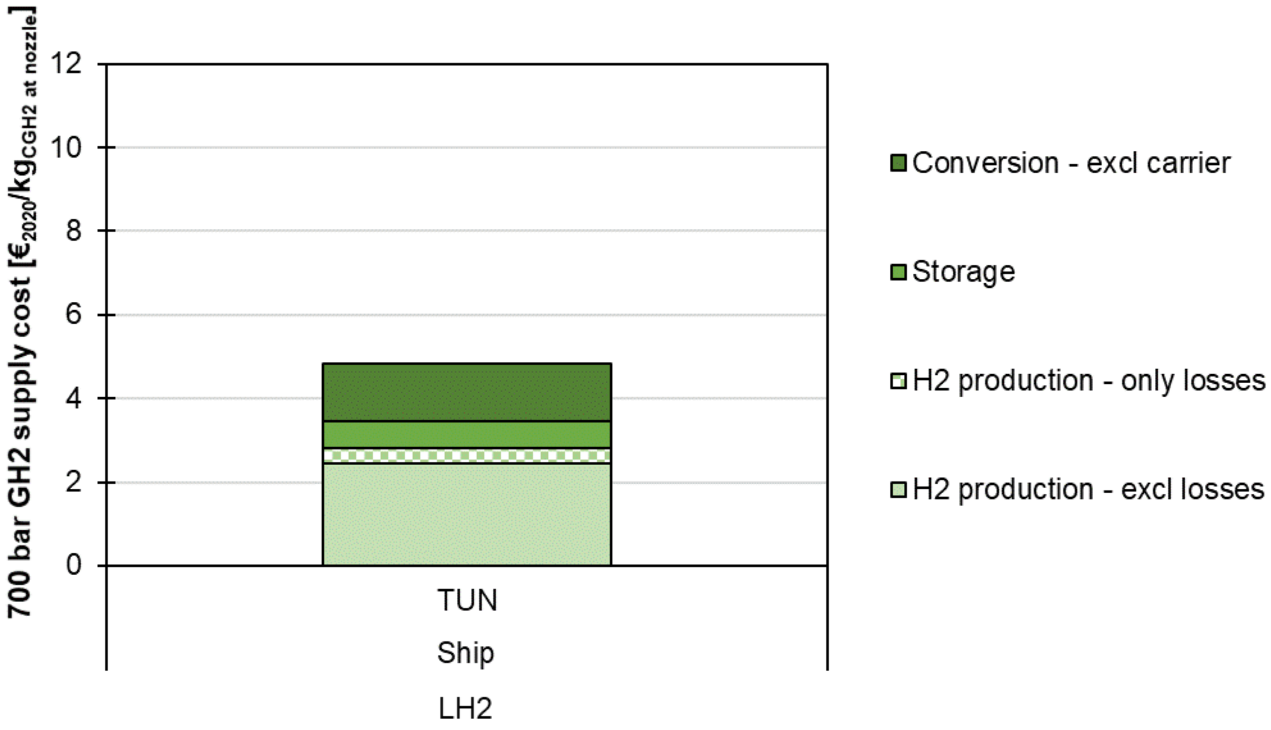

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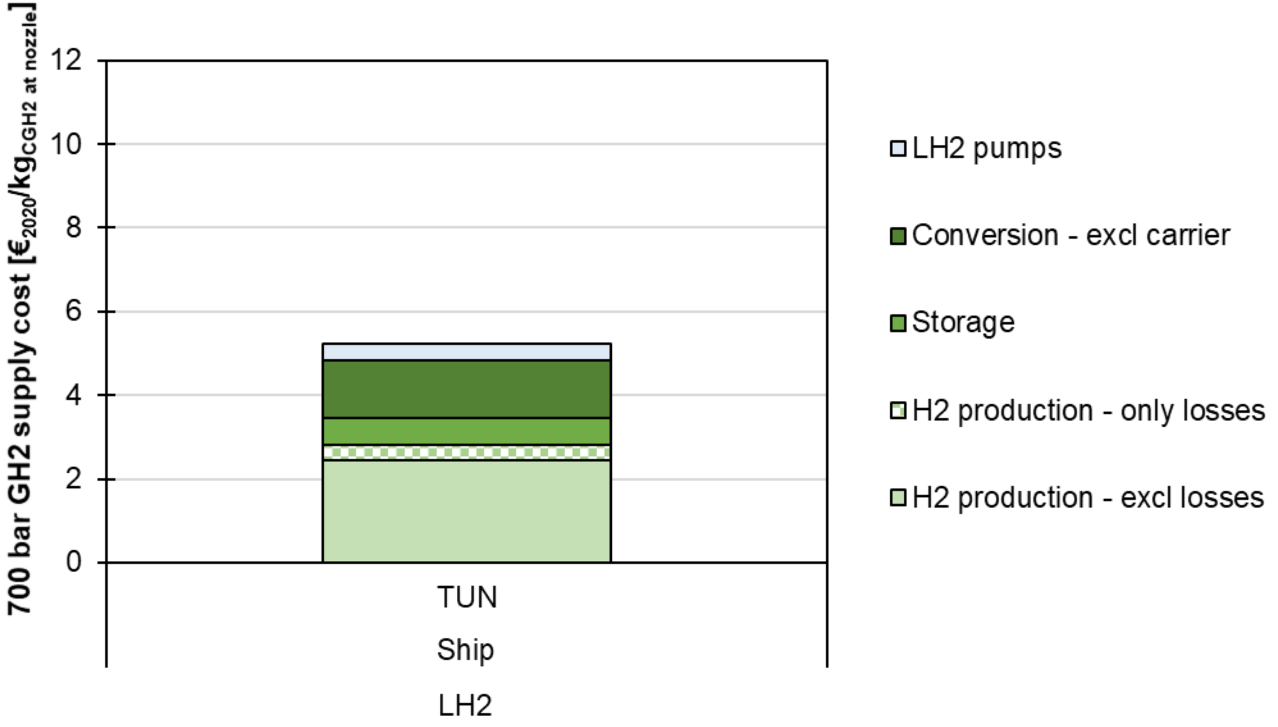

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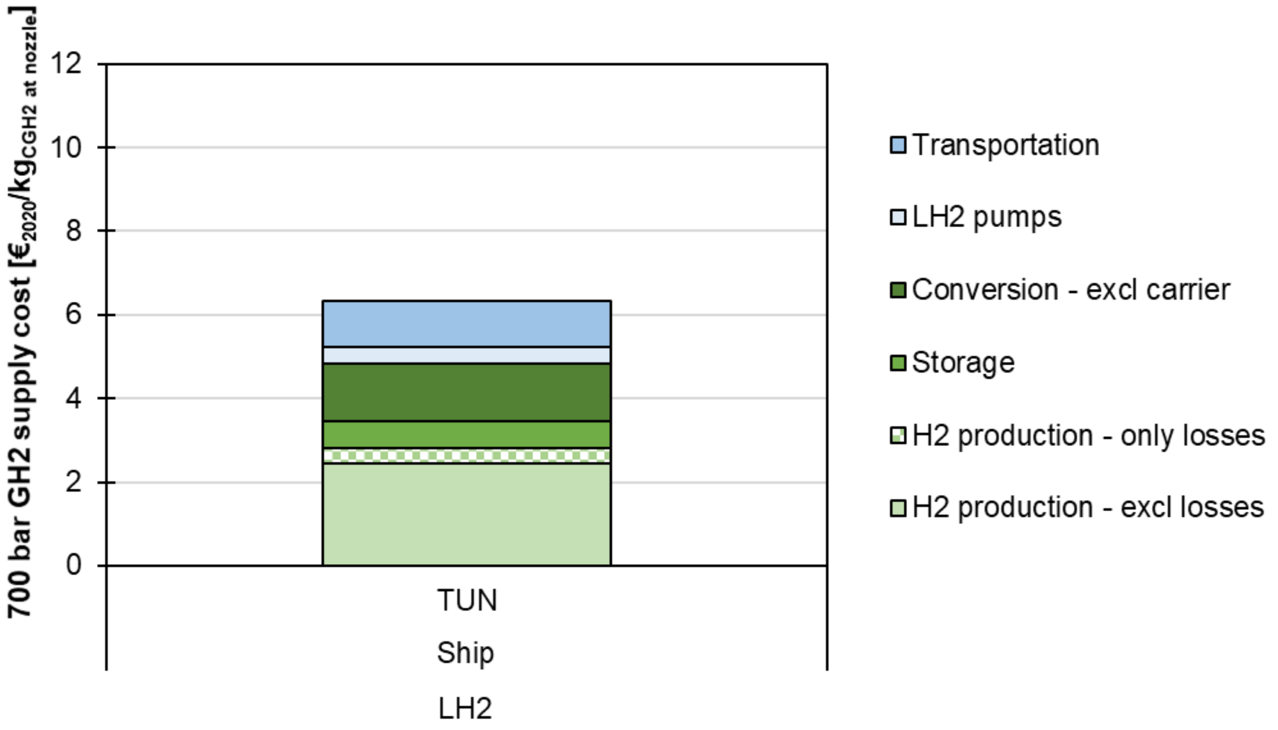

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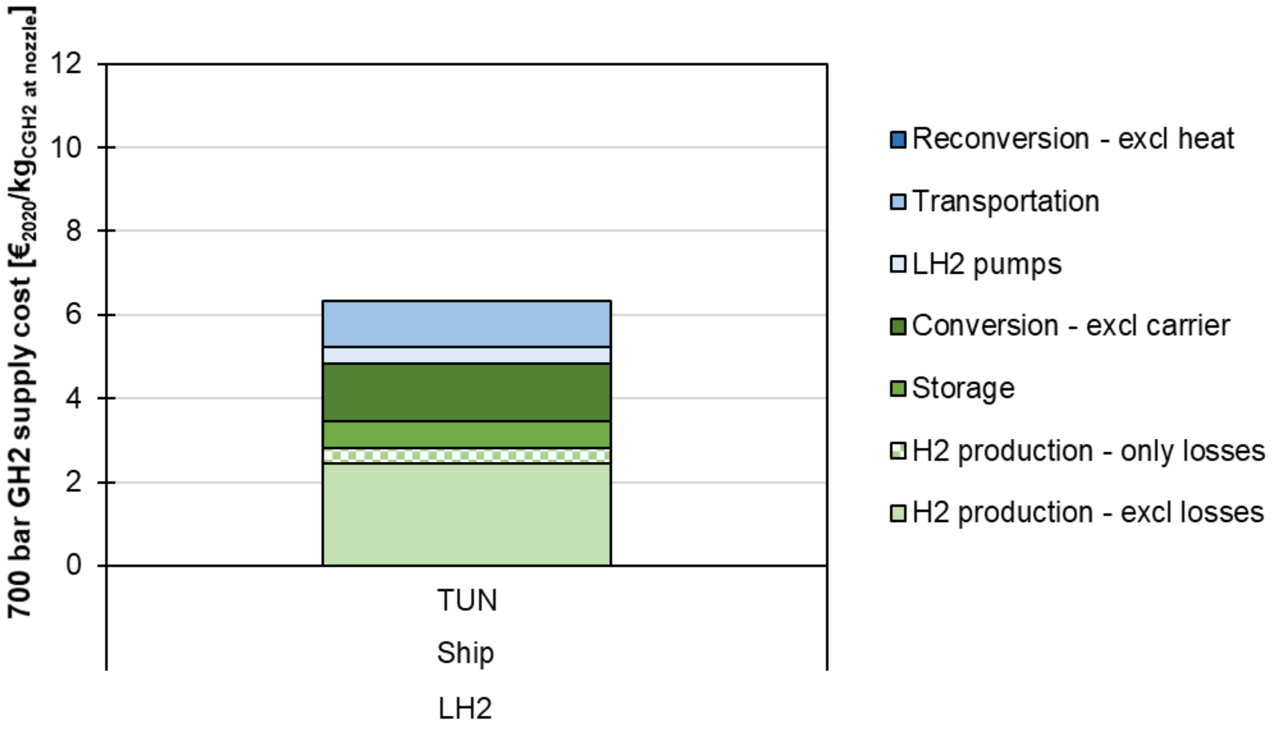

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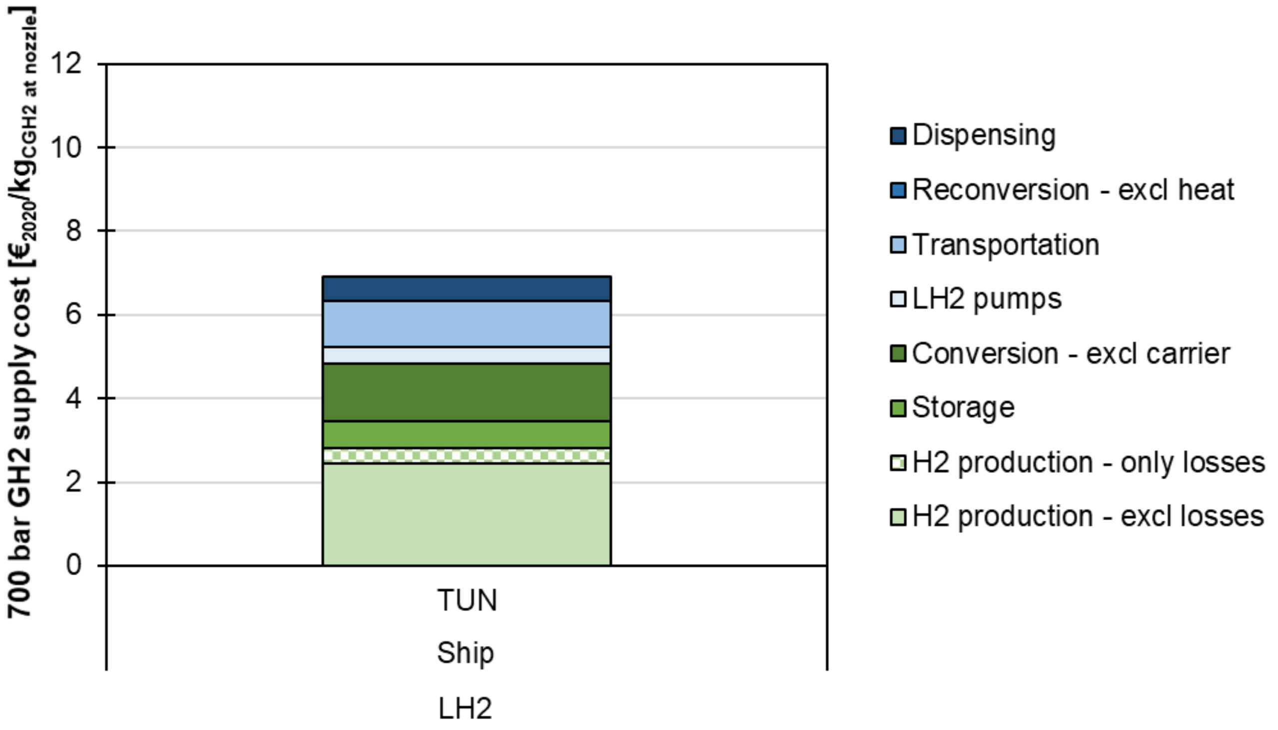

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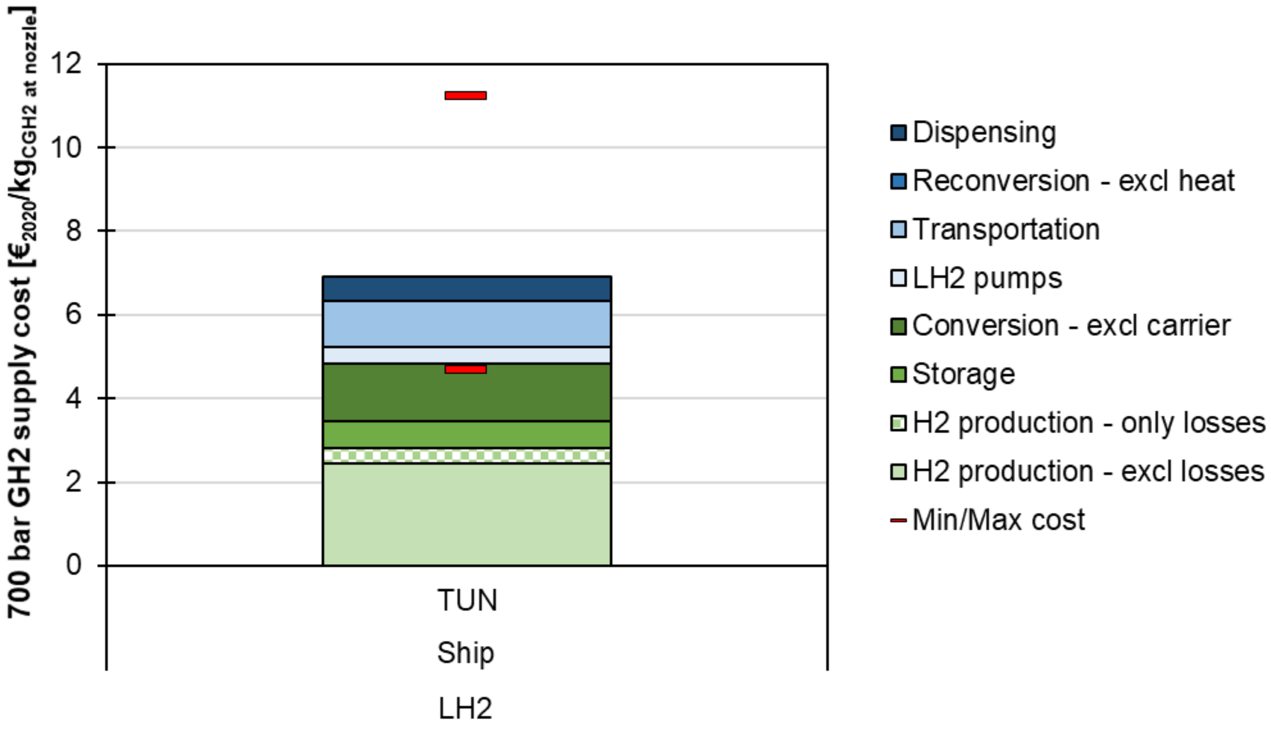

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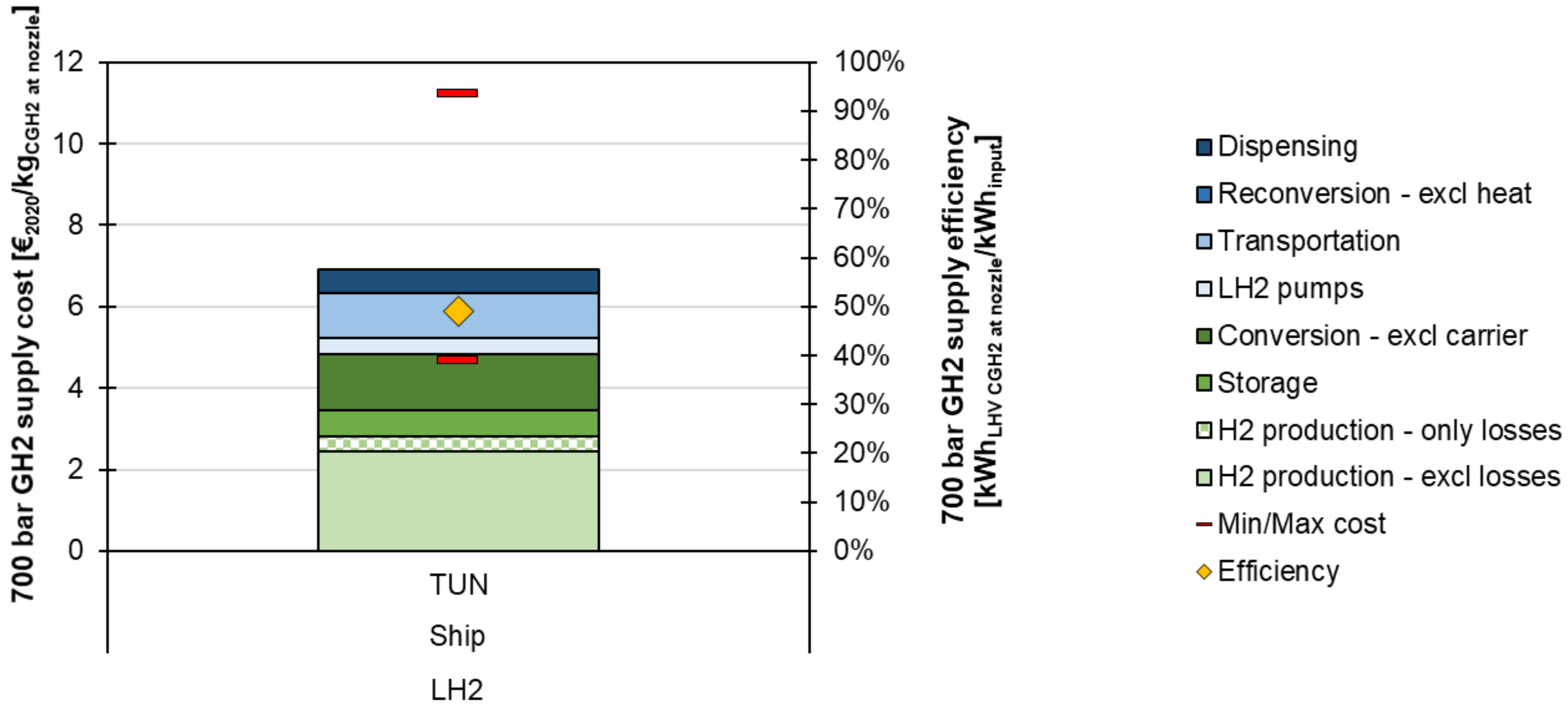
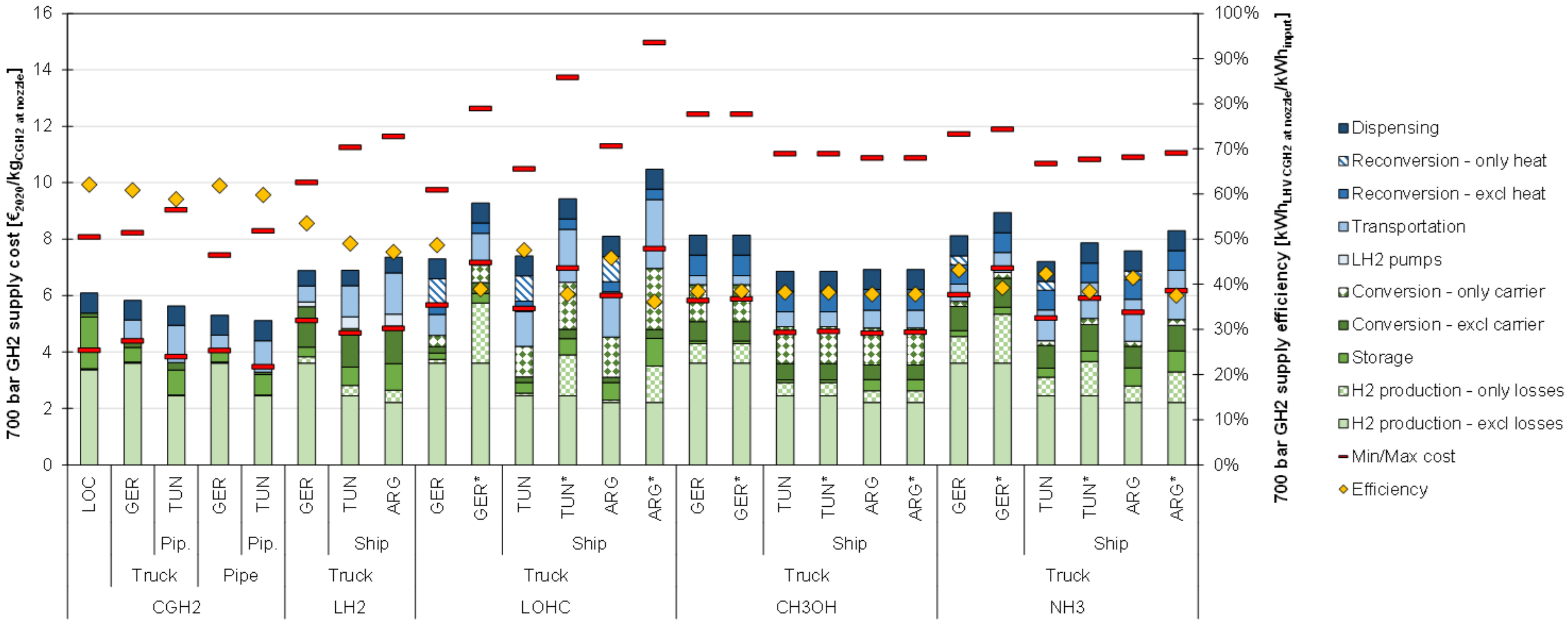
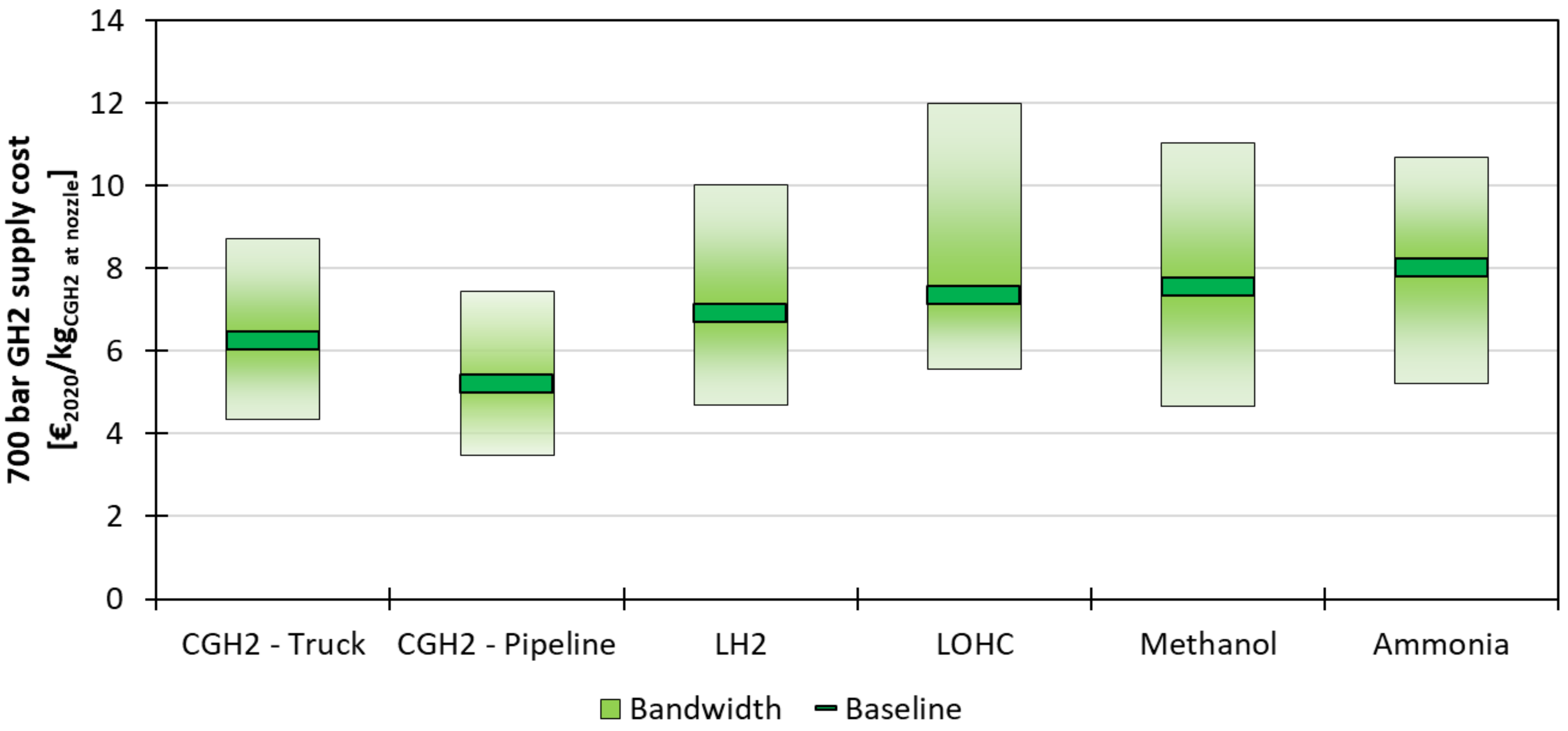


Gaseous Hydrogen Supply Cost in 2030

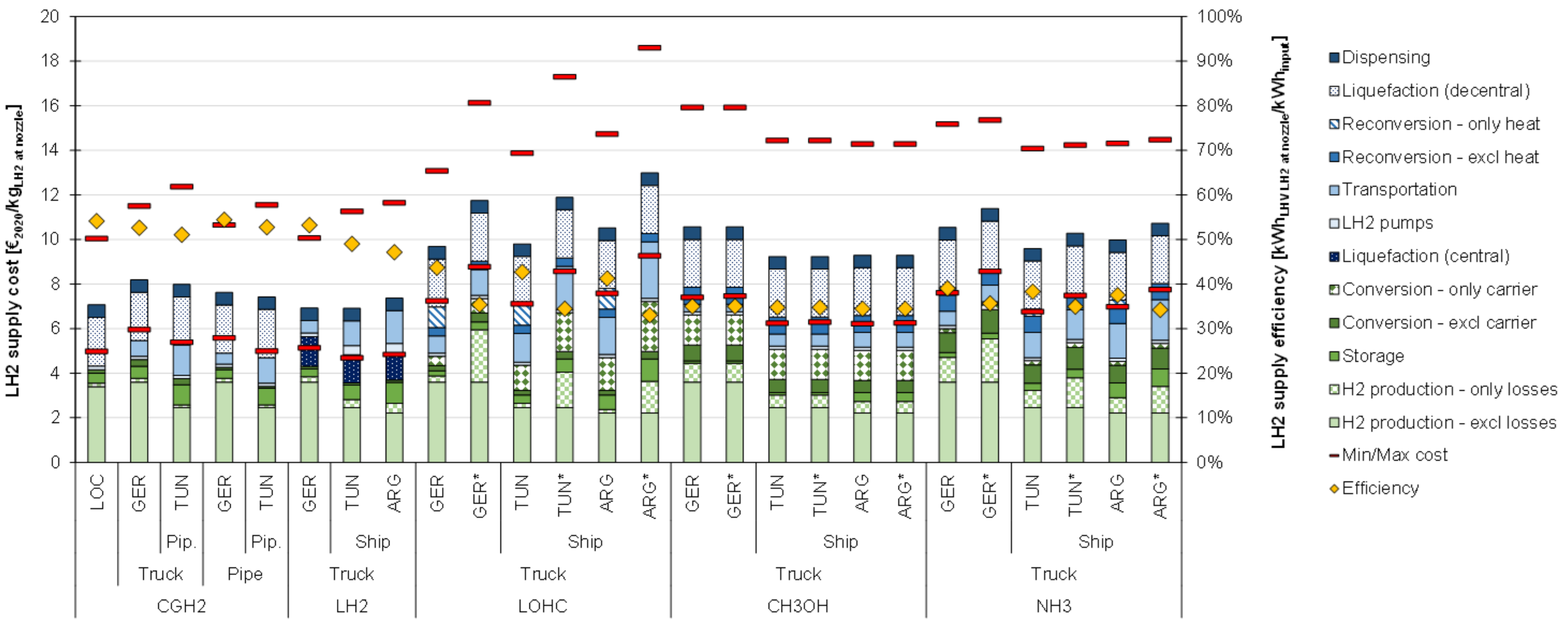


* Hydrogen is used for the dehydrogenation heat supply

Gaseous Hydrogen Supply Cost in 2030



Liquid Hydrogen Supply Cost in 2030



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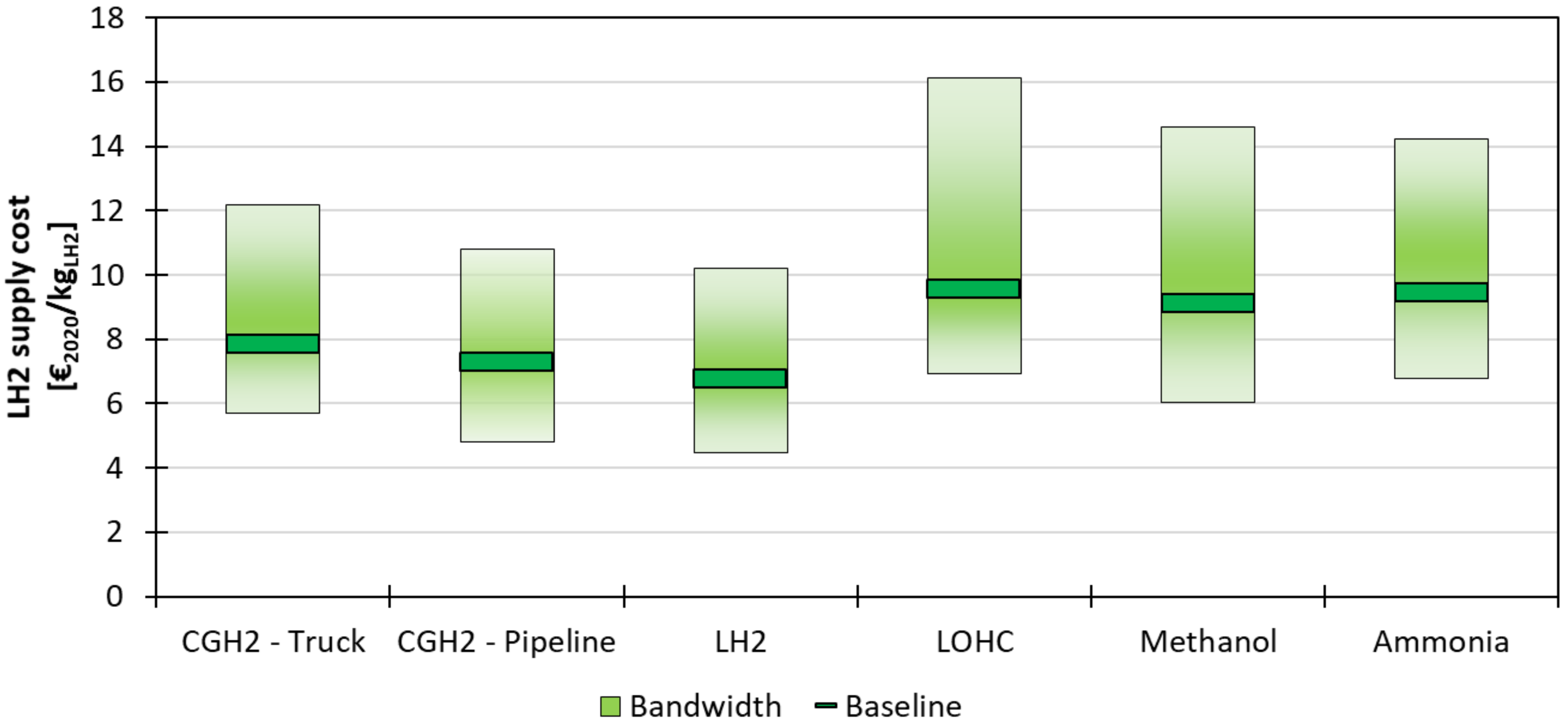
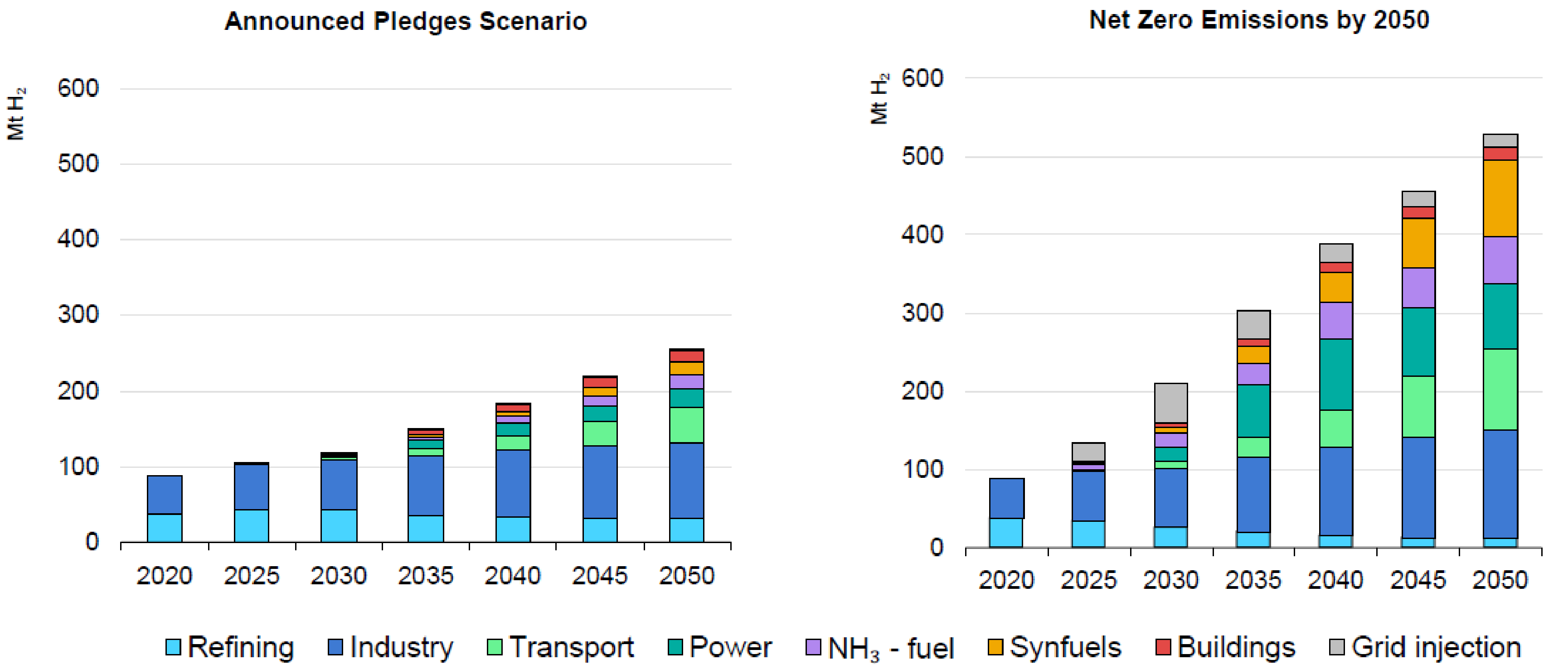
Liquid Hydrogen Supply Cost in 2030



Overview Hydrogen Utilization



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Heavy Duty Vehicles


[13]


[14]

- Faster refueling times reduces downtimes
- Lighter energy storage enables higher payloads
- Higher energy density offers longer ranges

⇒ Promising for multi-day, difficult-to-plan long-haul transport

Aviation and Shipping

[15]

[16]

- Energy efficient green fuel
- Lower supply cost than PtL fuels
- Enables stronger reduction of the global warming potential

→ Promising for short to midrange airplanes and vessels

Steel and Electricity Generation


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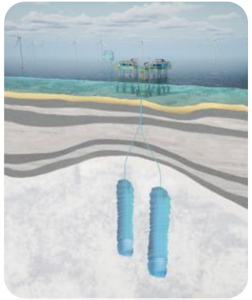
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[19]

- Direct iron reduction using hydrogen is seen as the most promising defossilization option for steel
- Salt cavern enables long time storage of renewable energy and with a subsequent electricity generation an uninterruptible power supply


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References

- Images slide 1, from left to right:
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  - [2] https://images.app.goo.gl/tgVUA1EQwqGEsxhm8
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  - [5] https://images.app.goo.gl/bD24v1L26ANsmx4n8
  - [6] https://images.app.goo.gl/58YNgjNLviaWJ1rZA
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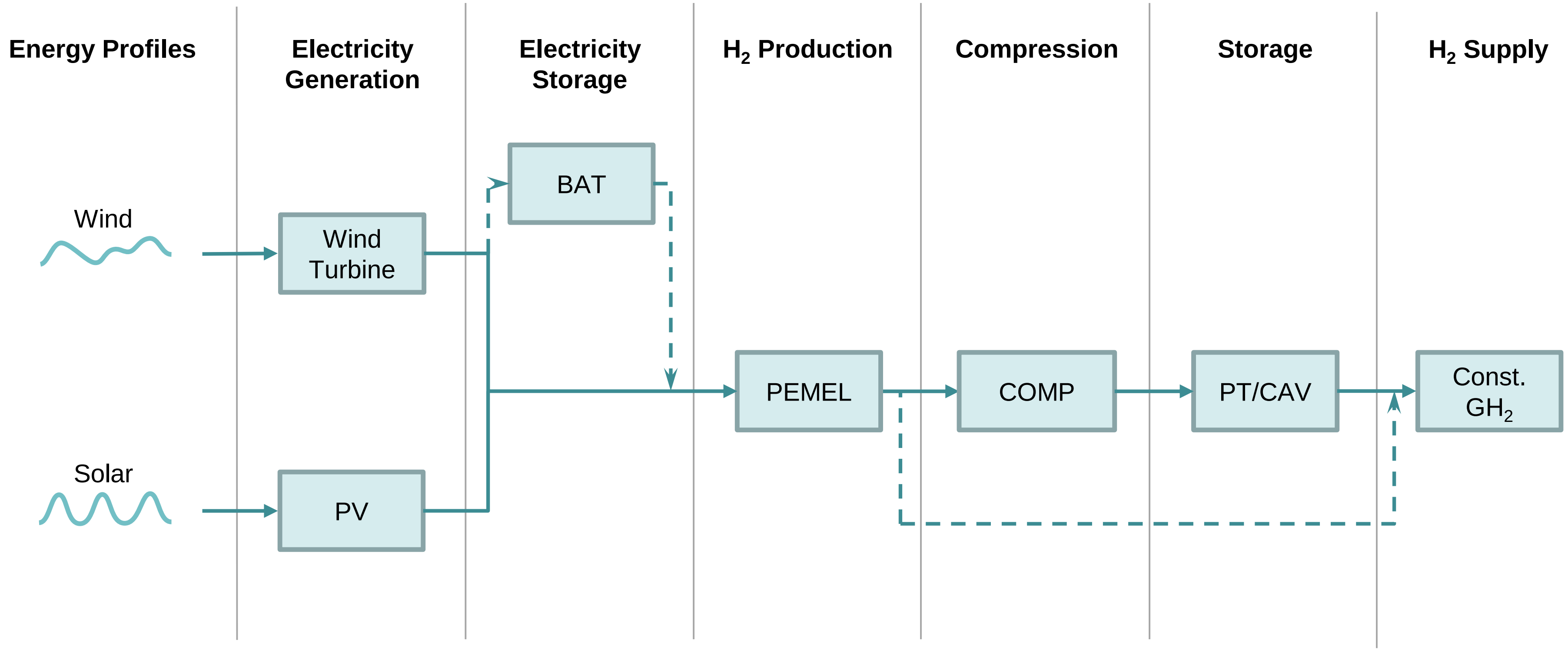
Detailed Supply Chains

Optimized Hydrogen Production



BAT = Battery; CAV = Cavern; COMP = Compressor; GH_2 = Gaseous Hydrogen; PT = Pressure Tank

Key Assumptions

	Year	PV	Onshore Wind	Offshore Wind	PEMEL
CAPEX [$€_{2020}/kW_{el}$]	2030	400 (310 – 570)	1,110 (1,010 – 1240)	1,890 (1,750 – 2,020)	860 (580 – 1,230)
	2050	270 (170 – 350)	990 (860 – 1,140)	1,620 (1,320 – 1,930)	510 (350 – 760)
Efficiency [$kWh_{H2,LHV}/kWh_{el}$]	2030	-	-	-	67% (63 – 69%)
	2050	-	-	-	71% (67 – 74%)

Seasonal storage capacities:

- Local (LOC) scenario: 15 days
- National (GER) scenario: 30 days
- Import (TUN & ARG) scenario: 60 days

Filling station capacity rate:

- Baseline: 50%
- Progressive: 60%
- Conservative: 40%

Technical Assessment

$$\eta_{supply\ chain} = \frac{q_{H2,nozzle}}{q_{overall}}$$

$$q_{overall} = q_{production} + q_{conversion} + q_{storage} + q_{transport} + q_{reconversion} + q_{fill}$$

$$q_{production} = q_{production,ideal} + q_{production,losses}$$

$$q_{compression} = \frac{R_s\, T_{comp}}{\eta_{comp}} \left[z_{out}\ \ln\left(\frac{p_{out}}{1.0135\ bar}\right) - z_{in}\ \ln\left(\frac{p_{in}}{1.0135\ bar}\right)\right]$$

Economic Assessment

$$c_{overall} = c_{production} + c_{conversion} + c_{storage} + c_{transport} + c_{reconversion} + c_{fill}$$

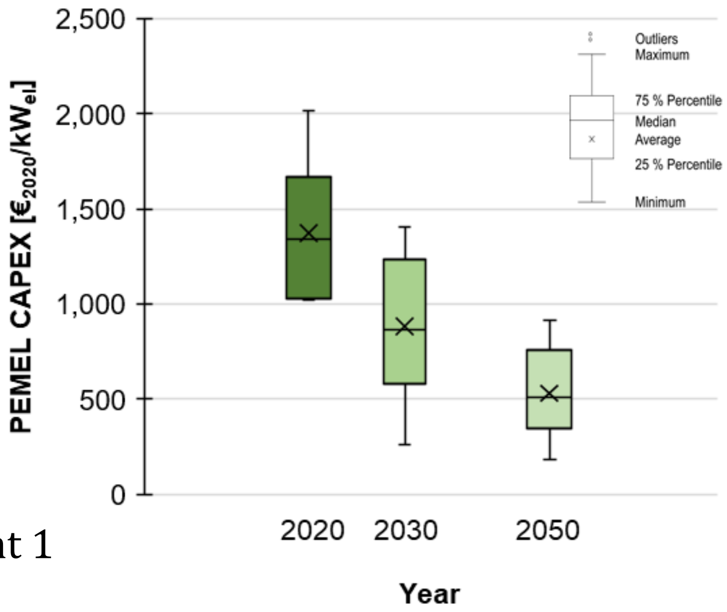
$$c_{section,i} = \frac{ACAPEX_i + OPEX_i}{m_{H2,fill,annual}}$$

$$ACAPEX_i = CAPEX_i \frac{WACC_{real}\,(1+WACC_{real})^{d_i}}{(1+WACC_{real})^{d_i}-1}$$

$$WACC_{real} = \frac{1+WACC_{nom}}{1+INFL} - 1$$

CAPEX Calculation

$$CAPEX_1 = f_{inst}\ f_{infl}\ CAPEX_{ref}\left(\frac{C_1}{C_{ref}}\right)^{\alpha}$$



- α = scaling factor
- C_1 = capacity of plant 1
- C_{ref} = capacity of reference plant
- $CAPEX_{1,inst}$ = installed 2020 € capital expenditure plant 1
- $CAPEX_{ref}$ = capital expenditure for reference plant
- f_{infl} = inflation factor (adjustmend to 2020 €)
- f_{inst} = installation factor (includes equipment, materials, construction and engineering)

LOHC CAPEX

$$c_{LOHC} = \frac{CAPEX_{LOHC}}{Cycle_{LOHC,annual}} \frac{WACC_{real}\,(1+WACC_{real})^{d_{LOHC}}}{(1+WACC_{real})^{d_{LOHC}}-1}$$

$$cycle_{LOHC,annual} = 8760 \frac{h}{a} / \; t_{LOHC,cycle}$$

$$t_{LOHC,cycle} = \sum_{i=1}^{n} t_i$$