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Anaerobic Digestion of Lignocellulose Components: Challenges and Novel Approaches

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Abstract: The reuse of lignocellulosic biomaterials as a source of clean energy has been explored in recent years due to the large amount of waste that involves human activities, such as those related to agriculture and food. The anaerobic digestion (AD) of plant-based biomass for bioenergy production poses a series of challenges that new technologies are attempting to solve. An improved decomposition of recalcitrant lignocellulose together with an increase in biogas production yield are the main objectives of these new approaches, which also seek the added value of being environmentally friendly. Recent research has reported significant progress in this regard, offering promising outcomes on the degradation of lignocellulose and its subsequent transformation into biomethane by specialized anaerobic microorganisms, overcoming the drawbacks inherent to the process and improving the yield of methane production. The future of the agri–food industry seems to be heading towards the implementation of a circular economy through the introduction of strategies based on the optimized use of lignocellulosic residues as a source of clean and sustainable energy.

Keywords: cellulose; hemicellulose; lignin; lignocellulose; plant biomass; methanogenesis; sustainability

1. Introduction

The search for sustainable energy sources to replace fossil fuels has led to focus attention on waste from human activities, the accumulation of which poses a serious threat to the sustainability of the production chain. Many of these residues have an important lignocellulosic composition. Specifically, agricultural waste and energy crops have gained much attention as candidate feedstocks for producing bioenergy production and biobased products [1]. The use of this residual biomass as an energy source has the potential to

improve the sustainability of agricultural and forestry systems and to reduce dependence on fossil fuels, decreasing greenhouse gas (GHG) emissions [2].

During the biological process of converting biomass into bioenergy, microorganisms degrade organic matter to yield biogas in the absence of oxygen. This technological process is known as anaerobic digestion (AD) [3]. However, the deconstruction of lignocellulose represents a biochemical challenge due to the complexity of their molecular structures. These plant-based materials are especially recalcitrant, consisting largely of cellulose and lignin polymers, which cause a physical impediment to the penetration of microbial enzymes, leading to sub-optimal degradation performance. Therefore, a pre-treatment prior to AD is a prerequisite for improving the biodegradability of lignocellulosic biomass [4]. Some issues related to the formation of inhibitory products, such as furans and phenols, or the high particle load, represent a problem for the adequate pre-treatment of biomass [5]. So, new protocols are being developed in order to counteract the deficiencies exhibited by the more classic procedures, also focusing on minimizing the associated environmental impacts (e.g., steam explosion, ozonolysis, ionic liquids (ILs), deep eutectic solvents (DESs), organosolv pre-treatment and supercritical fluids (SCFs)).

Although a good pre-treatment can facilitate a better degradation of the lignocellulosic biomass, other challenges inherent to AD itself are presented as a stumbling block to achieve advanced polymer decomposition, such as the accumulation of toxic compounds that inhibit bacterial activity, or the slow electron transfer through hydrogen or formate [6]. In this regard, new approaches such as genetic technology, static magnetic field, co-digestion of different substrates, the use of additives, and bioaugmentation, are being proposed to try to alleviate poor digestion of organic matter.

The aim of this article was to provide comprehensive information of how current anaerobic digestion methods of lignocellulosic materials affect biogas production as an alternative energy source. Recent and valuable information in this regard has been discussed throughout the manuscript, contributing with a description and important findings of the pre-treatments and digestion processes currently studied in a single work, focused on those residues from agri-food activities. Additionally, a definition and exhaustive description of the structure of lignocellulosic materials have been provided to assist in the understanding of the data presented.

2. Structure of Lignocellulosic Materials

Most terrestrial plants are constituted by three main polymers: cellulose (38–50%), hemicellulose (23–32%), and lignin (10–25%) [7]. Cellulose is the most important cell wall polymer, providing mechanical strength and chemical stability to plant materials [8]. The next quantitatively significant compound is hemicellulose. This polymer is chemically diverse and, as in the case of cellulose, primarily contributes to cell physical support [9]. Finally, lignin is the third major compound in plant tissues. This polymer has been found to provide different cell functions, such as water transport and stress resistance, helping also in plant stability [10]. Other compounds, including pectin, protein, extractives, and ash, are also present in small amounts in plant biomass and, depending on plant species, their composition, along with that of cellulose, hemicellulose, and lignin, can suffer variations [5]. Lignocellulose is a complex material with specific and intricate structures, which are described in detail in the following paragraphs.

2.1. Cellulose

Cellulose is a linear polymer made of D-glucopyranose ring units linked by β -(1,4)-glycosidic bonds, resulting in an alternate turning of the molecule chain axis by 180 °C [11]. All the repeating chains along the cellulose molecule are disaccharides (cellobiose) and are grouped in sub-structures of 20–300 units, conforming fibers. These long-chain polymers are then linked together by hydrogen and van der Waals bonds, promoting the packaging of cellulose into microfibrils [5]. Specific molecular ordering levels can be distinguished in these microfibrils, giving rise to different structural domains, such as crystalline (high-

ordered chains), paracrystalline (regions with loose molecular packing or some degree or crystal distortion), and non-crystalline (regions without regular packing of cellulose chains). Additionally, the presence of hydroxyl groups on the microfibril surface leads the appearance of cellulose–cellulose and cellulose–water interactions through a strong hydrogen bonded network, resulting in larger structures called “macrofibrils”, also known as “bundles” or “ribbons” [12].

2.2. Hemicellulose

The hemicellulose term groups a set of heterogeneous compounds, with an unknown molecular structure at the time this name was given. However, different structures were currently elucidated and, for this reason, the terminology is considered outdated and was suggested to be modified with little success [9]. Building blocks of hemicelluloses include pentoses (D-xylose and L-arabinose), hexoses (D-mannose, D-galactose, and D-glucose), hexuronic acids (4-O-methyl-D-glucuronic acid, D-glucuronic acid, and D-galacturonic acid), acetyl groups, and also small amounts of L-rhamnose and L-fucose. The abundance and structure of all these monomers are highly dependent on biomass sources [13]. Xylans and mannans are two prominent groups of hemicellulosic compounds, further divided into a set of structurally different polymers. Xylans comprise homoxylans, glucuronoxylans, arabinoxylans, and glucuronoarabinoxylans/arabinoglucuronoxylans, while mannans are classified in homomannans, galactomannans, glucomannans, and galactoglucomannans. Other compounds, such as xyloglucan, β -(1,3);(1,4)-glucan, and galactans, are also considered members of the hemicellulose family [13]. A brief description of these polysaccharides is provided below.

2.2.1. Xylans

Xylans are linear-structure polymers consisting of xylose residues linked by β -(1,4)-glycosidic bonds [14]. Depending on whether functional groups (4-O-methylglucuronic acid, glucuronic acid, arabinose, xylose, galactose, and glucose) are coupled or not to the molecule side chains, xylans can be categorized into hetero- or homoxylans, respectively. Specific functional group and its abundance will further classified heteroxylans in different hemicellulosic structures called glucuronoxylans, arabinoxylans, arabinoglucuronoxylans, or glucuronoarabinoxylans [13]. The backbone of glucuronoxylans is constituted by β -(1,4)-D-xylan, with the 4-O-methylglucuronic acid attached at the position 2 as the major substituent. However, glucuronic acid has also been found [15]. As the name suggests, arabinoxylans consist of arabinose as primary side groups attached at the position 2 or 3 along the xylose backbone. On the other hand, when heteroxylans contain both 4-O-methylglucuronic acid (and/or glucuronic acid) and arabinose in the xylose chain are called glucuronoarabinoxylans or arabinoglucuronoxylans [13].

2.2.2. Mannans

Two large groups of these polymers can be found depending on whether the β -(1,4)-linked backbone contains only D-mannose residues, which gives the name to these polysaccharides (mannans), or also D-glucose and D-galactose residues. Thus, homomannans consist of a single linear chain made up of β -(1,4)-linked mannosyl residues, whereas glucomannans and galactomannans also have β -(1,4)-linked glucosyl residues and α -galactose side chains attached to O-6 of some mannosyl residues, respectively. On the other hand, galactoglucomannans consist of a β -(1,4)-linked glucomannan backbone substituted with α -galactose at O-6 of some mannosyl residues [16].

2.2.3. Xyloglucans

These type of hemicelluloses are composed of β -(1,4)-linked glucose, with 75% of the molecule being substituted with α -(1,6)-linked xylose side chains [13]. Xyloglucans comprise a heterogeneous family of polymers of variable length and side chain pattern. In many plant species, the xyloglucan backbone has a regular pattern of three substituted

glucose units followed by an unsubstituted glucose residue. Conversely, in some taxonomic groups, substitution occurs less frequently [17].

2.2.4. β -(1,3);(1,4)-glucan

The backbone of β -(1,3);(1,4)-glucan comprises a linear structure formed by β -D-glucopyranose residues linked by means of β -(1,3) and β -(1,4) glucosidic bonds [18]. Cellotriosyl and cellotetraosyl units [made up of β -(1,4)-linked glucose residues] are linked together by a single β -(1,3)-glucose residue [19].

2.2.5. Galactans

Galactans are a broad family of hemicelluloses very widespread in the marine environment, mainly represented by agars and carragenans. Two large groups of these polymers have been identified: sulfated galactans and arabinogalactans, with different molecular structures. Sulfated galactans are a variable set of heterogeneous compounds with specific configurations, but with a conserved backbone made of α -L-and/or β -D-galactopyranosyl units. In the case of arabinogalactan, its main backbone consists of (1,4)-linked β -D-galactopyranosyl with short side chains of (1,5)-linked α -arabinofuranosyl attached in O-3 position [20]. The structure of lignocellulosic materials has been shown in Figure 1 [21].

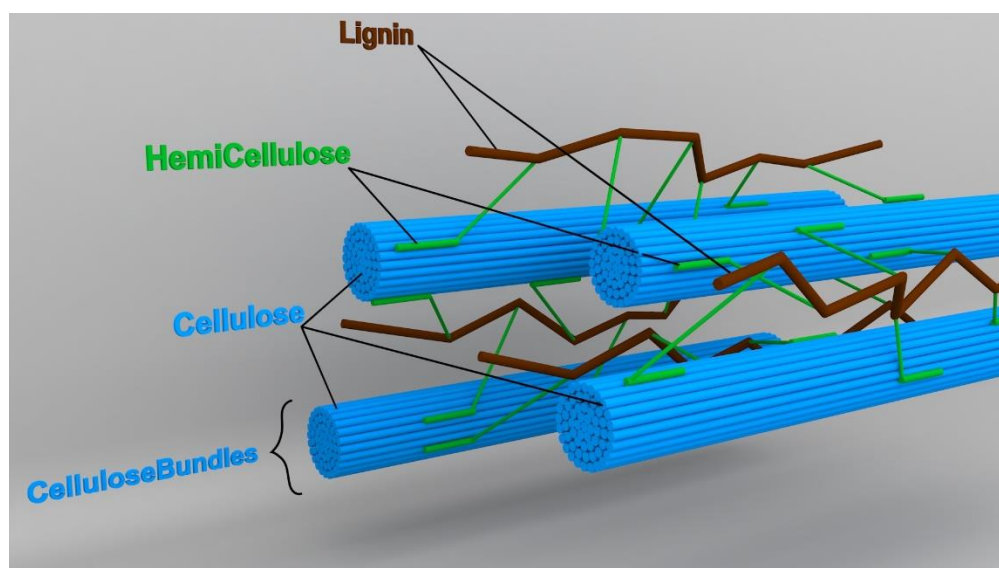


Figure 1. Structure of Lignocellulosic Materials.

2.3. Lignin

Lignin is considered the most complex fraction of the lignocellulosic materials found in nature [8]. It contains a long-chain backbone made up of three phenyl propane units. Namely: coniferyl alcohol (guaiacyl propanol), coumaryl alcohol (p-hydroxyphenyl propanol), and sinapyl alcohol (syringyl alcohol), linked together through alkyl-aryl, alkyl-alkyl, and aryl-aryl ether bonds [5]. Different proportions of these monomers in the lignin molecular chain lead to a wide range of polymers [22]. The structure of lignin polymer has been shown in Figure 2. Lignin cellulose and hemicellulose concentrations of lignocellulosic and food materials has been presented in Table 1.

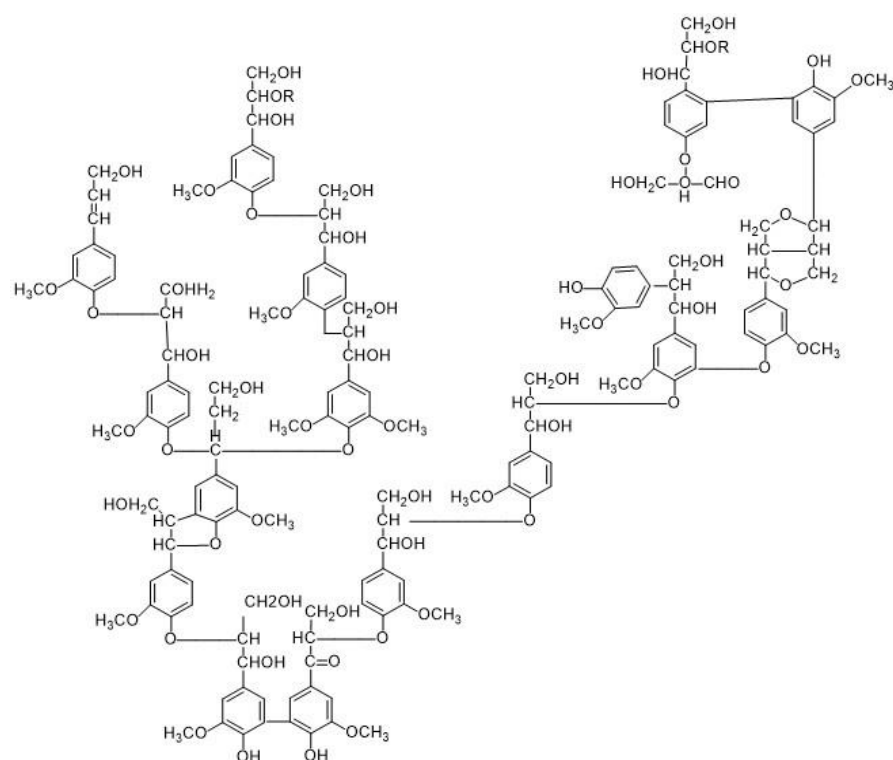


Figure 2. Structure of Lignin.

Table 1. Cellulose, hemicellulose, and lignin contents in different types of agri-food biomass [23,24].

Biomaterial	Chemical Composition (% DW)		
	Cellulose	Hemicellulose	Lignin
<i>Fruits</i>			
Black currant	12	25.3	59.3
Grape	30.3	21	17.4
Olive	36.4	26.8	26
Prickly pear	27	–	2.5
Cherry pomace	12	10.7	–
Pear pomace	34.5	25.3	59
Tamarind kernel	10–15	55–65	–
Apple waste	7.2	24.4	23.5
Banana waste	13	15	24
<i>Cereals</i>			
Barley hull	24	36	19
Barley Straw	36–43	24–33	6.3–9.8
Corn cob	32.3–45.6	39.8	6.7–13.9
Corn stover	35.1–39.5	20.7–24.6	11.0–19.1
Oat husks	23	35	25
Oat Straw	31–35	20–26	10–15
Nut shells	25–30	22–28	30–40
Rice husk	28.7–35.6	11.96–29.3	15.4–20
Rice Straw	29.2–34.7	23–25.9	17–19
Sorghum Straw	32–35	24–27	15–21
Wheat bran	10.5–14.8	35.5–39.2	8.3–12.5
Wheat Straw	35–39	22–30	12–16
Winter rye	29–30	22–26	16.1

Table 1. Cont.

Biomaterial	Chemical Composition (% DW)		
	Cellulose	Hemicellulose	Lignin
<i>Other biomaterials</i>			
Bamboo	49–50	18–20	23
Coffee pulp	33.7–36.9	44.2–47.5	15.6–19.1
Cotton	85–95	5–15	0
Cotton stalk	31	11	30
Oilseed rape	27.3	20.5	14.2
Sugarcane bagasse	25–45	28–32	15–25
Sugar beet pulp	27.4	28.1	3.1
Sugarcane tops	35	32	14

3. AD of Lignocellulosic Materials

AD processes naturally occurring in anoxic environments, such as watercourses, sediments, or waterlogged soils [25], where biomass is biochemically degraded by anaerobic bacteria in the strict absence of oxygen, generating methane and carbon dioxide as final reaction products [26,27]. Through the understanding of parameters involved, the anaerobic transformation of organic matter can be controlled, offering significant advantages over other processes intended for waste recycling, such as the reduction of biomass sludge production [25], use of the digestion final residue as fertilizer [28], or cost-effective energy recovery with low environmental impact [29]. Nevertheless, some critical points have been reported in the anaerobic treatment of waste, including long-term microbial stabilization, close control of parameters (pH, temperature, and feed rate) [29,30] or the need for post-treatment of the digested material before being released to the environment [31].

Anaerobic treatment of lignocellulosic matrices has recently become an excellent way to valorize organic wastes derived from a wide range of highly produced human activities, providing high energy recovery, with minimal environmental impact [32]. Agricultural residues are readily accessible sources of biomass that are produced in large amounts during harvesting and food processing. These highly organic-content materials are an excellent biologic fuel for obtaining energy, thus promoting sustainability and the circular economy. Suitable bacterial degradation of lignocellulosic materials depends on a series of complex and difficult optimizing variables. In this regard, improving stable and efficiency biogas production represents a challenge for the renewable energy industry. The following sub-sections provide an updated description of the most recent discoveries and strategies in the field of AD to obtain green energy from lignocellulosic biomass.

3.1. Pre-Treatment of Lignocellulosic Biomass Prior to AD

Optimum biogas production from lignocellulosic materials encompasses a series of perfectly delimited stages during microbial fermentation. Polymers should be firstly hydrolyzed and solubilized to be fully disposable for bacteria. Otherwise, organic matter conversion to biogas will be compromised. When it comes to degrading lignocellulosic polysaccharides, molecular ordering of polymeric structures is a key factor to consider. While amorphous cellulose is easily digestible, crystalline cellulose is resistant to bacterial attack. Cellulose in nature is predominantly found in crystalline disposition, adaptive feature of plants to defend themselves against attack of fungi and bacteria [33]. The specific organization of glucose polymers in this type of cellulose, disposed in directional cellodextrin chains that assemble into large and long microfibrils, enables a very compact and crystalline system, compromising the access of anaerobic bacteria to the interior of molecule [34]. The complex structure of lignin, already commented in the present review, have also showed to be a physical barrier difficult to overcome for microbial enzymes. In addition, the formation of lignin-carbohydrates complexes further restrict polysaccharide accessibility. On the other hand, non-productive binding with enzymes have been reported [35]. Definitely, lignin is the most recalcitrant lignocellulosic compound of the

plant cell wall [36], and together with cellulose form a toughly attackable matrix by bacteria. Therefore, plant-based materials should be pre-treated before AD to ensure the highest possible substrate conversion. According to biomass characteristics (i.e., crystallinity of cellulose and polymerization degree, lignin composition, and degree of hemicellulose acetylation), pre-treatment must be carefully chosen, aimed at obtaining optimal biogas production. In this regard, different approaches have been proposed, leading to the development of physical, chemical, and biological methods, successfully used in biomaterials. Nevertheless, issues, such as the formation of inhibitory products (e.g., furans and phenols), high particle load, or high energy input, have been reported to occur [5], suggesting that better pre-treatment protocols need to be proposed. In addition, the strong acids and alkalis used in traditional delignification processes did not provide good quality substrates for the subsequent fermentation stage [37]. In this regard, a recent study carried out the optimization of a low-temperature delignification protocol in *Platanus acerifolia* leaf residues for the production of bioethanol. Green reagents, such as acetic acid and hydrogen peroxide, replaced other more dangerous and environmentally harmful reagents, achieving a satisfactory removal of lignin. Moreover, the use of mild operation temperatures enhanced the energy efficiency of the process [38].

3.1.1. Novel and Green Pre-Treatment Methods

Steam Explosion

Novel technological applications have recently been investigated addressed to replace conventional methods, such as alkaline and acid pre-treatments, recognized for a long time [39]. One of the current, but already relatively well-established green pre-treatment methods, is steam explosion. Water steam is applied on the lignocellulose components at high temperature for few minutes in order to facilitate its enzymatic hydrolysis to monomeric hexose and pentose sugars. The addition of acid has been found to enhance the process performance [40]. Residual organic matter from food industrial processes, such as the crushed agave heads in the tequila production [41,42], mesocarp tissues during the elaboration of food and coconut-based beverages [43], or the straw after wheat harvesting [44], have been successfully steam pre-treated. After applying pressures around 0.5–4.8 MPa at temperatures in the interval of 160–260 °C, pressure is sharply reduced, which causes an increase in the specific surface area and pore size [45], improving the substrate biodegradability and subsequent energy recovery through the stimulation of gas production. Although, cellulosic fractions and lignin are effectively break down under this pre-treatment, high temperatures (above 160 °C) were found to produce toxic derivatives [46], such as phenols, furans, and acetic acid [47], inhibiting the subsequent anaerobic fermentation process [48]. A post-pretreatment detoxification step is then required.

Wet Explosion

Wet explosion is an innovative pretreatment technique, which was patented in 2004 [49]. It is the combination of wet oxidation and steam explosion. The lignocellulosic material can be pretreated at different severity conditions by adjusting temperature, pressure and oxygen concentration [50]. Lignin is considered as a primary challenge in the anaerobic digestion of lignocellulose. The wet explosion pretreatment has been found quite effective in overcoming the lignin challenge during anaerobic digestion. Some of the recent studies has shown that the lignin polymer of lignocellulosic materials can be degraded effectively if the material is pretreated by Wet Explosion pretreatment before anaerobic digestion [22,49,51]. Methoxylation of lignin polymer can improve its degradation under anaerobic conditions and wet explosion pretreatment improve the methoxylation of lignin polymer [52].

Ozonolysis

Ozone has been reported to be effective in degrading lignin with minimum and null affectation on hemicellulose and cellulose structures, respectively [39]. This colorless and unstable gas is recognized as a strong oxidizing agent [53], which decomposes into radicals

and reacts with organic matter both directly and indirectly through the hydroxyl ion [54]. Ozonolysis of wastewater from alcohol distilleries was recently found to increase the biogas production yield while reducing GHG emissions. Pre-treatment of an organically complex wastewater from a molasses-based distillery under this procedure provided a substrate with enhanced AD, resulting in favorable biohydrogen release (production rate of 1.18 mL/h) [55]. Ghorbani et al. [56] reported the ozone flow rate and residue moisture as the most contributing factors in wheat straw delignification. In connection with this, Ariunbaatar et al. [57] suggested optimal ozone doses in the range of 0.05–0.5 g O₃/g. In contrast to steam explosion, pre-treatment with ozone leaves no residue in the system.

ILs

With the term “Ionic liquid”, we refer to the product resulting from mixing certain ionic species [39]. These solvents have unique thermal, physical, chemical, and biological properties, such as low viscosity, extremely low vapor pressure, or long-thermal stability [58]. ILs were found to be able to dissolve specific substances of interest such as lignocellulosic biomaterials, allowing to reduce their recalcitrance [59] and increasing bioenergy production. In addition, these liquids are considered environmentally friendly alternatives to organic solvents, as they are clean (without hazardous residues derived from their application), recoverable after used, non-toxic, non-corrosive, and biodegradable [60,61]. Different kinds of ILs, such as 1-ethyl-3-methylimidazolium acetate, choline lysinate, and ethanolamine acetate, have been successfully tested on agave bagasse resulting from tequila production for its solubilization and breakdown, providing high sugar yields and increasing anaerobic digestibility. IL–water mixtures yielded results comparable to those obtained using pure ILs, thus improving process profitability while allowing easier handling by decreasing viscosity [62]. Specifically, choline lysinate offered the highest yield of sugar production (0.57 g total sugars/g biomass), reaching a similar result when diluted up to 30% in water. Pérez-Pimienta et al. [63] reported a similar result for the same IL on identical residue (0.51 g total sugar/g biomass). Pre-treated solids produced up to 7.5 times more methane/g chemical oxygen demand than the untreated solids. Significantly lower sugar release was reported by using the IL 1-ethyl-3-methylimidazolium acetate on solid post-harvest materials. A lignocellulosic biomass: IL ratio of 1:5 w/w only reduced the crystallinity of wheat straw and grape stem by 5%, with no further increase in methane production. The mild conditions of the pre-treatment were found to be responsible for the low hydrolysis achieved, which highlights the importance of a good process optimization [64]. In this regard, the use of the IL in biorefineries entails the challenge of controlling a number of critical parameters, which include the election of the solid loading, temperature, or the need for a co-catalyst to enhance the hydrolysis capability [39]. Regardless of all the advantages exhibited, the high viscosity, which makes handling operations difficult, and cost, are blocking the large-scale implementation of ILs as a pre-treatment method in AD processes [61].

DESs

The search for cheaper and greener pre-treatments with ILs led to another class of alternative solvents called “deep eutectic solvents”. These liquids share several physico-chemical properties with ILs, considered analog solvents, such as the intricate hydrogen bonding network [65]. DESs can be easily prepared by mixing Lewis or Brønsted acids and bases that can contain a variety of anionic and/or cationic species, while ILs are composed primarily of one type of discrete anion and cation [66]. Choline chloride is frequently used as a hydrogen bond acceptor, combined with carboxylic acids or glycols as hydrogen bond donors [65].

The affectation of biomass structure by DESs was recently explored in rice straw by analyzing the different lignocellulosic fractions. Pre-treatment with choline chloride/urea mixture showed a higher selectivity on lignin, exhibiting an efficient solubility. In contrast, α -cellulose crystallinity increased during the process due to a deconstruction of the hydrogen bond networks [67]. The limited DES action on cellulose was reported to be related

to its scarce ordered molecular conformation, which limits the entropy gain and leads to a poor biomass dissolution [68]. Conversely, lignin and hemicellulose have been found to be deeply affected by DESs. Oh et al. [69] reported significantly increased sugars from these lignocellulosic fractions compared to cellulose during the pre-treatment of pine wood, suggesting that the polarity and hydrogen bond acidity of DESs can be behind this result, as determining factors in the extraction of hemicellulose and lignin from biomass. The breakdown of the lignocellulose pre-treated with DES enabled better biomethane productions in different types of substrates [65,70,71]. Thus, despite still being a little-explored solvent for the lignocellulose pre-treatment, advantages, such as the ability to dissolve lignin and hemicellulose, low cost, and scarce toxicity, make DASs attractive elements to be used in the framework of a new concept of greener and more sustainable biorefineries.

Organosolv Pre-Treatment

Organosolv pre-treatment is a recent and one of the most efficient and promising pre-digestion processes applied for lignin removal from plant-based biomaterials. This pre-treatment involves the use of an organic solvent (organosolv) or its aqueous solution, such as a short-chain aliphatic alcohol (e.g., methanol and ethanol), polyhydric alcohol (e.g., glycerol, ethylene glycol, and triethylene glycol), alkylene carbonate, organic acid, or other (e.g., acetone and ILs). These solvents are mixed with the lignocellulosic biomass and the set is then heated at a temperature between 100 and 200 °C for a short period of time (30–150 min) [72–74], thus enabling the lignin solubilization, along with a part of the hemicellulose fraction, leaving the cellulose in the solid state [75]. The temperature of the process may be reduced by means of a catalyst, which will depend on the type of biomass [76].

Organosolv pre-treatment has been tested on several food industry by-products, such as, potato peel, corncob, and olive wastes, for obtaining bioenergy, resulting in improved biomethane production rates prior feedstock delignification [77–79]. Despite recent advances in this regard, mainly focused on the use of ethanol as an extraction solvent, organosolv pre-treatment is currently a poorly understood process and the glucan purities obtained from non-wood materials are still limited [73]. Therefore, further research should be carried out in an attempt to optimize the recovery of a glucan-rich solid fraction.

SFCs

SFC technology is gaining interest as an alternative and environmentally sustainable technology to other more conventional technologies in industry. Supported in its unique physicochemical properties (intermediate between those of a gas and liquid), it has been already tested in a wide range of dissimilar industrial applications, such as the extraction of compounds, particle formation, formulation of new materials, and impregnation of aerogels, among others [80].

A wide variety of agri-food biomass, such as corn stover [81], corncob [82], rice straw [83], wheat straw [84], or sorghum stalk [85], has been pre-treated with supercritical CO₂. The use of this green solvent for biomass pre-treatment has showed to enhance glucose yield, delignify, and hydrolyze the hemicellulose fraction, also enabling the extraction of compounds [86]. In addition, carbon dioxide causes the acidification of the environment by reacting with water and forming carbonic acid, which helps in the hydrolysis of hemicellulose and breaks of intra H-bonds between cellulose, hemicellulose, and lignin [87]. An interesting advantage of using carbon dioxide is the possibility of recycling that produced during the digestion stage to be used in the pre-treatment [86], which might lead to a significant increase in the profitability of the total process. Some of the recent studies about all the above-mentioned pretreatment techniques has been presented in Table 2 and the effect of pretreatment on lignocellulosic materials and their conversion during anaerobic digestion has been shown in Figure 3.

Table 2. Innovative pretreatment techniques to enhance degradation of lignocellulosic materials under anaerobic digestion.

Feedstock	Chemical Used	Pretreatment Conditions	Methane Yield	Reference
<i>Ionic Liquids Pretreatment</i>				
Agave bagasse (AB)	1-ethyl-3-methylimidazolium acetate [Emim][OAc]	119 °C, 142 min	-	[62]
Agave bagasse (AB)	choline lysinate [Ch][Lys]	160 °C, 205 min	0.28 L CH ₄ /g COD _{fed}	[62]
Agave bagasse (AB)	ethanolamine acetate [EOA][OAc]	160 °C, 90 min	-	[62]
Agave bagasse (AB)	choline lysinate [Ch][Lys]		0.26 L CH ₄ /g COD _{fed}	[63]
<i>Steam Explosion Pretreatment</i>				
Coffee husks (CH)	-	210 °C, 15 min	292 NmL CH ₄	[88]
Birch wood	-	220 °C, 10 min, 18–20 bar	566 mL/g VS	[89]
Rice Husk	-	224 °C, 2.53 MPa, 5–7 min	199 mL/g	[90]
Agave bagasse	-	240 °C, 0.68–0.98 MPa, 22 min	316–362 mL g COD _{fed} ^{−1}	[91]
<i>Wet Explosion Pretreatment</i>				
Biorefinery lignin.	0–2% NaOH	220 °C with 4% oxygen	195.4 ± 2.3 mL/gVS/day	[21]
Feedlot manure	-	170 °C for 25 min, 4 bars oxygen	320 ± 36 L/kg-VS/Day	[51]
<i>Organosolv Pretreatment</i>				
Potato peel wastes (PPW)	50–75% (v/v) Ethanol	120–180 °C	57.9 L biomethane/kg waste	[78]
Napier grass	50% (v/v) aqueous ethanol	190 °C for 15–60 min	410 mL/g-VS	[92]
Hazelnut skin (HS)	50% (v/v) water-methanol solution	130–200 °C	310.6 mL CH ₄ /g VS	[75]
Biodegradable fraction of municipal solid waste (BFMSW)	85% aqueous ethanol	120 °C for 30 min	31.7 L methane/kg	[93]
<i>Ozonolysis</i>				
Sugarcane bagasse	7.5 mgO ₃ gSB ^{−1}	-	252.1 NmL gSV ^{−1}	[94]
Macroalgae <i>Ulva latuca</i>	8.3 mg O ₃ min ^{−1}	-	498.75 mL/g VS	[95]
<i>Supercritical CO₂ explosion</i>				
Sewage Sludge	-	115 °C and time of 13 min	300 mL CH ₄ /g VS	[96]
<i>Euglena gracilis</i>	-	30–50 °C, 300 bar, 2 h	456 mL g ^{−1} VS	[97]
<i>Phaeodactylum tricornutum</i>		30 MPa, 30 °C, and 30% ethanol	56.7 L CH ₄ /kg VS	[98]
<i>Deep eutectic solvents</i>				
Organic Fraction of Municipal Solid Wastes (OFMSW)	ChCl:OA (1:1)	60 °C	593 mL	[65]

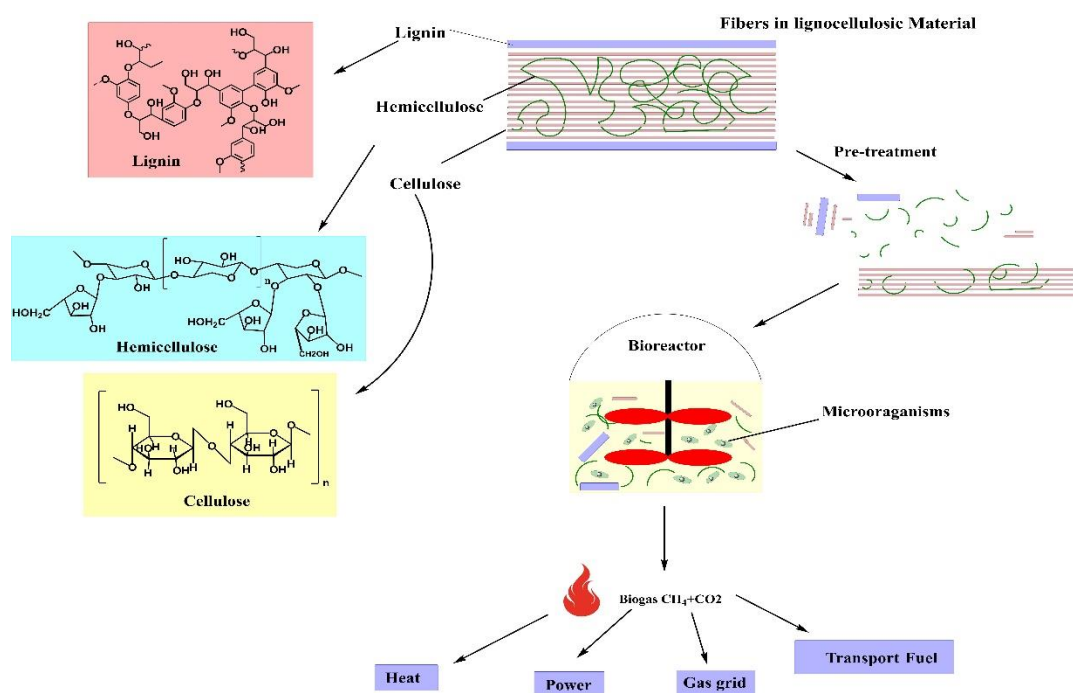


Figure 3. Effect of pretreatment on lignocellulosic materials and their conversion during anaerobic digestion.

3.2. AD of Lignocellulosic Biomass

3.2.1. Concept and Process Stages

Once the pre-treatment of the lignocellulosic biomass has succeeded in reducing the structural and compositional constraints, microbial enzymes can more easily access the glycosidic bonds during the AD stage and further break down the exposed and partially degraded polymers of cellulose, hemicellulose, and lignin, leading to the production of renewable biogas. This biogas is mainly composed of methane and carbon dioxide in 50–75% and 25–50% approximate proportions, respectively [3]. In addition, other minor gases, such as hydrogen sulfide, nitrogen, hydrogen, ammonia, and water vapors have also been reported [99]. Therefore, AD is considered a biological and often complex process, occurring throughout a number of chronological and chemically differentiated steps, classified in hydrolysis, acidogenesis, acetogenesis, and methanogenesis and carried out by a different microbial functional group. Namely: hydrolytic, acidogen, and acetogenic bacteria, and methanogenic archaea [100].

- Hydrolysis

When anaerobic bacteria access to the interior of the partially degraded biomass, they secrete extracellular enzymes that further decompose this biomass to simple soluble monomers in amino acids, fatty acids, and sugars [100]. In other words, insoluble organic materials and higher molecular mass compounds are transformed into soluble organic materials; suitable to be used as a source of energy and cell carbon [26]. Different types of hydrolytic bacteria have been found to be involved in this first digestion step, giving rise to different molecules, such as via amino acids via proteinase, cellobiose and glucose via cellulase, glucose via amylase, or fatty acids and glycerol via lipase [26].

- Acidogenesis

All the aforementioned monomers obtained by hydrolysis are now converted into intermediate compounds, such as short-chain and volatile fatty acids (VFAs) (propionic, butyric, propionic, and acetic acid) and other minor products (alcohol, hydrogen, and carbon dioxide) by fermentative bacteria (acidogens) [3,26,100].

- Acetogenesis

The short-chain fatty acids produced in the acidogenesis step are then the substrate for those called acetogenic microorganisms, giving rise to acetate, carbon dioxide and/or hydrogen, and providing substrates for methanogenesis, the last step of the AD process [100,101].

- Methanogenesis

Finally, methanogenic archaea use acetate, carbon dioxide, and hydrogen as a substrate, releasing methane. Two subgroups within the methanogens are involved in this final digestion stage. Aceticlastic methanogens produce methane from acetates, while hydrogenotrophic methanogens produce it from carbon dioxide and hydrogen [102,103]. Methanogens are believed to have the slowest growth rate among microbial population involved in AD, being also highly sensitive to changes in environmental conditions, such as temperature, pH, and the concentration of inhibitors [100]. Different stages of the anaerobic digestion process have been shown in Figure 4.

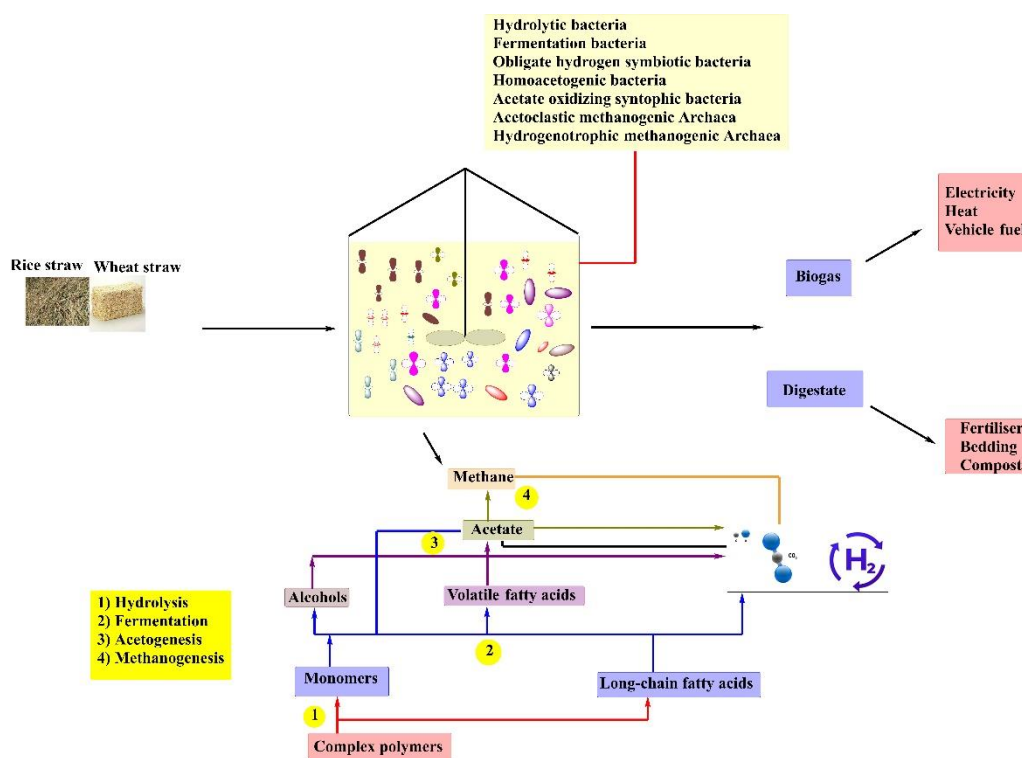


Figure 4. Different stages of anaerobic digestion of waste materials and their conversion to electricity.

3.2.2. Future Directions and Opportunities

During AD, a series of challenges, such as VFAs and hydrogen accumulation, which may be toxic for methanogenic and acetogenic bacteria, or the slow electron transfer through hydrogen or format, need to be faced [6], since they restrict biogas production. Novel approaches, such as genetic technology, static magnetic field, co-digestion, the use of additives, and psychrophilic AD, have recently been addressed in order to counteract the aforementioned drawbacks and improve AD efficiency. Principles and foundations of these new strategies, as well as their effective application in agri-food waste, have been deeply discussed in the following paragraphs.

Genetic Engineering for Biogas Production

Genetic tools have recently played a fundamental role in improving specific crop traits. Resistance to some diseases and to an adverse climate, or the simple modification of certain sensory attributes in the plant or fruit, can be achieved through the alteration of specific

genes. Similarly, the intricate molecular structure of the plant cell wall may be modified by removing or suppressing the expression of the genes involved. This will give rise to a less recalcitrant biomass and will ease the action of microbial enzymes during the hydrolysis step without affecting plant cell viability [104]. Another possible strategy would be to influence the metabolic activity of the microorganisms responsible for the degradation of lignocellulosic material, improving their ability to break down this polymer framework and release sugars [105].

Although both criteria are viable and potentially applicable, genetic engineers have opted for reconfiguring the lignocellulosic backbone of the plant cell wall as the primary approach rather than influencing in the hydrolytic capacity of bacteria. However, modifying a system naturally designed to support and protect plants could interfere with the proper development of their structures. For this reason, it is necessary to establish a compromise between resistance and ease of biodegradation that provides new individuals with a more easily hydrolysable but functional cell wall [106].

Influencing the disposition of lignin monomers is essential to reduce the recalcitrance of lignocellulosic materials, since this biomass fraction is especially inaccessible for hydrolytic enzymes. The different proportion of the monomers that configure the lignin molecule (*p*-hydroxyphenyl propanol, guaiacyl propanol, and syringyl alcohol) provide polymers with distinct digestibility [107]. Thus, the abundance of syringyl alcohol units has been found to favor the digestibility of the lignin molecule by constituting a less condensed structure than its counterpart composed of guaiacyl propanol units. While the first of the mentioned configurations has been associated with cell wall and reinforcement functions, the second might be responsible for functions such as plant defense [108]. Tetreault et al. [109] identified the gene that encodes the activity of the enzyme responsible for the biosynthesis of syringyl alcohol in the sorghum plant. Overexpression of the *sbF5H* gene, under the control of the CaMV 35S promoter, enhanced the action of ferulate-5-hydroxylase (*F5H*), leading to an increase in syringyl alcohol units and the syringyl alcohol/guaiacyl propanol ratio in the lignin molecule without hardly affecting the plant growth and development. Similarly, Hodgson-Kratky et al. [110] initiated the search for genes and markers associated with the syringyl alcohol/guaiacyl propanol ratio in the lignin molecule of the sugarcane plant. These authors identified 2019 differentially expressed transcripts among genotypes with different syringyl alcohol/guaiacyl propanol ratios, which, together with the identification of specific alleles expressed with the phenotype, could lead to obtaining plant varieties with a lignocellulosic structure less resistant to microbial digestion.

The reduction in cellulose recalcitrance is also a factor to consider in the genetic redesign of plant biomass. It is evident that the modifications in the polymers of this molecule must be aimed at favoring an amorphous structure that leaves more spaces for the access of cellulases. Recent studies have intentionally manipulated genes directly involved with the molecular ordering of cellulose in the rice plant [111–113], giving rise to mutants with a less crystalline cellulose. On the other hand, genes related to the formation of the cellulose molecule have been reported not to compromise normal plant growth [114].

Genetic engineering may also contribute to improving biomass degradability by altering the microbial capacity to produce more robust hydrolytic enzymes. The low catalytic activity and yield of cellulases, together with their poor thermostability, usually hinder the sugarification of lignocellulosic residues. The progress made in recent years has helped overcome these limiting factors, improving the kinetics and efficiency of these microbial enzymes [115]. Similarly, genes that regulate lignin degradation metabolic pathways have been manipulated or edited in order to improve bioconversion efficiency. There are several promising lignin-degrading organisms for use in synthetic biology or metabolic engineering, such as *Pseudomonas putida* and *Corynebacterium glutamicum*, which have already been cultivated on an industrial scale for commercial purposes. The application of metabolic engineering on other organisms such as *Rhodococcus* and *Amycolatopsis* is still under development [116]. In *P. putida*, strategies such as expanding the specificity and assimilation of substrate and the improvement of the chemical production derived from lignin depolymer-

ization (generation of phenolic compounds of interest) are used to improve the efficiency of lignin valorization [117].

The so-called metabolic engineering in microbes is the current most advanced approach to influence the regulation of enzymatic expression of a specific cellular pathway linked with other signaling pathways [118].

Impulse of Lignocellulosic Digestion by Application of a Static Magnetic Field

Recently, the external application of a magnetic field has been shown to be an efficient strategy to promote the biodegradation of organic matter [119]. Although the mechanism of action is not yet well-elucidated, there are studies that suggest alterations in the cellular activity of certain microorganisms, with a supposed special magnetic susceptibility, when they are exposed to a magnetic field, affecting growth and metabolic functions [120]. Static magnetic field at low flux density has been shown to be especially biostimulant [121,122], concretely at a density below 50 mT [123]. While a density above 100 mT has been found to affect cell viability [124]. However, the greatest germicidal effect is achieved through the use of a pulsed magnetic field, which is presented as an alternative to thermal sterilization treatments [125].

The application of a static magnetic field during the AD of agri-food biomass has resulted in an increase in the microbial population, leading to enhanced methanogenesis. Zhao et al. [126] observed an increase in the concentration of methanogen organisms after the induction of a static magnetic field at a flux density of 11.4 mT in corn stover. Under this magnetic intensity, the authors reported an increase of more than 80% in the microbial population, including archaea of the order methanocellales, the main group of methane-producing archaea found in the decomposition stage.

The idea of the magnetic field as a strategy to improve biogas production is not yet very widespread. There are only a handful of published studies on the subject. Nevertheless, the results are promising. In addition, it is considered a clean, non-toxic, and safe technology [127].

Co-Digestion of Various Substrates to Overcome Biodegradability Limitations

The simple strategy of combining two or more substrates in the digestion reactor has been seen to correct the biodegradability deficiencies of each of the substrates individually. This simultaneous digestion of biomass, known as co-digestion, therefore improves energy production by increasing nutrient availability to microbes and organic load, while reducing chemical toxicity by diluting each of the substrates [128,129]. In addition, there may be a promotion in microbial diversity [130].

Despite the high amount of nutrients present in agriculture residues and algae, the recalcitrant nature of their tissues represents an obstacle in the biodegradation process. However, when these materials are co-digested with others of dissimilar nature, such as animal manure or other organic substances, the final biomass obtained offers greater access to microbials, promoting improved degradation [131]. Velásquez Piñas et al. [132] demonstrated that the digestion of corn and grass ensilage with cattle manure can provide better performance in terms of size and consumption of electricity and heat compared to the individual digestion of the substrates. On the other hand, the deficient amount of carbon found in animal waste can thus be remedied, reaching an adequate carbon:nitrogen (C:N) ratio. Half cow manure to oat straw (1:2) was found to be a suitable relation for AD of this mixture, which provided a C:N ratio of 27. This proportion also guaranteed a good rate of lignocellulose degradation and subsequent methane production, releasing a 25% more than during mono-digestion of plant material [133]. An identical C:N ratio (26–27.5) also provided excellent methane production during co-digestion of agro-industrial waste material (hay grass and wheat straw) with an animal residue such as chicken litter. A ratio slightly higher than 1:2 (chicken litter:agro-industrial waste) was found to optimize the performance of the organic matter degradation process [134].

As can be seen, the co-digestion of raw materials shows to be a useful tool in the revaluation of agro-waste for the generation of bioenergy. Nevertheless, this strategy entails risks associated with the continued availability of substrates, the complexity of the organic matter owing to its different recalcitration, and safety issues when using products such as animal manure. On the other hand, determining an optimal ratio between feedstocks to be digested is still considered a challenge, as it is conditioned by factors, such as the nature of the material, composition, content of trace elements, and biodegradability, among others [130].

Addition of Additives to Improve Lignocellulosic Digestion

The use of additional compounds, including metal elements, carbon-based accelerants, biological additives, and alkalis, during AD treatments has been shown to significantly increase degradation performance and biogas release, as well as reduce air pollution during the process. Each additive offers specific and unique advantages in improving biogas production and their incorporation into digestion reactors is therefore a promising approach. Nevertheless, crucial aspects such as dosages, effects and applications remain still unknown [135].

- Metal elements

Metal elements promote the fermentation of substrates through the formation of the active center, cofactor, and structure of the enzymes involved in digestion [136]. The presence of metals, such as Fe, Co, Ni, Zn, Mo, W, and Se have been reported to play an important role in obtaining adequate performance during the anaerobic degradation of raw material [137]. The addition of Fe^{2+} was observed to improve hydrolysis and acidification reactions in coffee husks wastes, significantly increasing the concentration of intermediate compounds in methane production. Additionally, the observed cooperation between Fe^{2+} and other ions, such as Ni^{2+} and Co^{2+} , resulted in enhanced enzymatic activity of methanogens [138]. In another experiment, supplementation of chicken manure leachate with trace elements, including Se, Co, W, Mo, Ni, Zn, Mn, and Fe, offered a 36.5% higher yield of methane production [139].

Maintaining a stable and efficient conversion of organic matter requires an appropriate supply of metal ions. However, physicochemical conditions during digestion (pH and redox potential) and the reaction kinetics of chemical processes occurring both in liquid (reduction, precipitation, or complexation) and solid (absorption) phases will significantly influence the speciation and chemical bioavailability of trace elements [140]. These factors need to be considered when designing the experiment, as well as the type of substrate, which will require a specific metal at a given concentration. On the other hand, an excessive concentration of metal ions in the digester can inhibit the decomposition process [135]. It is therefore absolutely necessary to understand all the parameters that can affect the correct function of metal elements during the degradation of feedstocks in order to obtain an adequate concentration that leads to optimal energy production.

- Carbon-based materials

In other types of studies, carbon-based materials are assessed as enhancers of AD, and have been found to be capable of modifying the microbial environment, producing significant improvements in organic matter conversion. Their declared physicochemical advantage (e.g., fine pore structure, good electrical conductivity, large porosity, and surface area) contributes to a superior microbial development and improved biogas release. Recent research has successfully tested distinct types of these carbon accelerators in the revaluation of residues with lignocellulosic fractions. Wu et al. [141] reported that the addition of graphene to the reactor can improve methane production from thin stillage by 11%. The authors attribute this performance to the high conductivity of graphene. Qi et al. [142] suggested that this carbon-based material is able to promote direct electron transfer between *Pseudomonas* and *Methanosaeta*, accelerating the methanogenic pathway of carbon dioxide reduction and achieving a higher methane production. In general, carbon conductive

materials are widely used to increase the direct interspecies electron transfer (DIET) [143]. During this electrochemical process, electrons are transferred directly from donors to acceptors through microbial nanowires, cytochromes, and conductive materials and have been suggested to be involved in acetogenesis, acetate oxidation, and methanogenesis [144]. The addition of carbon nanotubes promote DIET among acetogenic and methanogenic microorganisms, thus increasing microbial activity and shortening the digestion process by means of an accelerated acclimatization to the environmental conditions of the reactor [143]. An amount of 500 mg/kg of this carbon nanomaterial improved the AD of sheep manure, increasing the release of methane by more than 30%. During the degradation process, the microbial composition was altered at the genus level, particularly those members of *Methanobacterium*, which increased their relative abundance by up to 120% [145,146]. The supplementation of raw materials with inorganic nanomaterials has been reported to enhance the efficiency of AD due to physicochemical properties, such as their high surface area and number of active sites or their high reactivity and specificity. In addition to carbon-based nanomaterials, other nano-sized materials (1–100 nm), namely zero-valent metallic nanoparticles, metal oxide nanoparticles, and multi-compound nanoparticles, can also be introduced into the reactors [147].

The product resulting from the carbonization of lignocellulosic waste, known as biochar, has been intensively explored in recent years as a promoter of the AD process [148]. This product is a precursor of activated carbon obtained by thermochemical conversion under conditions of extreme oxygen limitation [149]. The addition of biochar to the digester has been reported to produce a significant improvement in the degradation of lignocellulose from plant materials, such as corn, wheat, and rice straw, sorghum, and potato pulp [150–152]. This stimulation of the digestive process may certainly address the difficulties inherent in the recalcitrance of plant biomass and ensure adequate stability into the reactor. Certain aspects, such as the enhancement of the hydrolysis reaction, the balance among acidogenesis and acetogenesis, the reduction in the accumulation of VFAs or the favoring of methanogenesis, have been attributed to the action of biochar [153].

The use of this carbon-based material has the added value of being produced from the pyrolysis of lignocellulosic waste, contributing to the recycling of waste materials originated in different agri-food activities. Moreover, coupling biochar production to an AD operation can achieve an economically advantageous system with positive environmental performance [148].

Activated carbon has also been found to be an ally in the anaerobic decomposition of lignocellulose [154,155]. The inhibition caused by high concentrations of ammonium can be avoided by incorporating this product into the reactor, facilitating AD under conditions of ammonium stress [156,157]. Activated carbon is the result of an activation process in a carbon-rich material. Plant residues can be used instead of coal as an alternative production method, making the transformation process more profitable [76]. The review article by Hassan and coworkers clearly and thoroughly explains the formation of this carbon-based material [158,159].

Psychrophilic AD

It is well-known that temperature is a limiting factor during fermentation processes. Low temperatures often lead to long digestion cycles and poor biogas production [160]. However, it is necessary to consider the energy expenditure involved in the use of adequate temperatures for the action of mesophilic and thermophilic microorganisms during anaerobic decomposition processes, between 30 to 40 °C and 50 to 60 °C, respectively [161]. Maintaining these temperatures makes feedstock processing difficult for small companies. For this reason, they usually operate at room temperature [162]. Similarly, the use of mild temperatures may also be more economically profitable in cold and high-altitude regions, with temperatures barely above 20 °C [163].

After testing different approaches to improve anaerobic degradation performance under psychrophilic conditions, including substrate pre-treatment, co-digestion of feedstock

with another, and addition of certain additives (all strategies discussed in this review), the bioaugmentation has proven to be the most direct procedure to achieve this target [164]. The acclimatization of mesophilic bacteria before their inoculation in the reactor is the most used strategy in low-temperature ADs [165,166]. This procedure was studied using methanogenic archaea during the co-digestion of corn straw and cattle manure at a controlled temperature of 20 °C. Xu et al. [151] inoculated different concentrations of a propionate-degradation culture (mainly composed by *Methanothrix* and *Methanobacterium* archaea) previously acclimated to this temperature in order to improve the AD performance under psychrophilic conditions. The addition of 14% of the mentioned microbial group was found to significantly increase biogas production. However, a significantly lower addition (4%) provided the best bioaugmentation efficiency. This study demonstrated that through the inoculation of microorganisms adapted to a psychrophilic environment digestion performance can be improved, alleviating the accumulation of VFAs, especially acetate and propionate.

Low temperatures seriously limit the AD process by conditioning the microbial growth of mesophiles and thermophiles and their enzymatic activity. However, the use of psychrophiles could solve these problems as they have evolved in cold environments, enabling the development of a variety of genotypic and phenotypic adaptive features [162]. The use of cold-adapted lignocellulose-degrading microbial complex community LTF-27 at an operating temperature of 15 °C yielded a hydrolytic conversion rate of 22.64% in corn straw and a methane production of 204.72 mL/g, higher than that obtained in the control group (121.19 mL/g). The improved balance of energy consumption achieved in this study demonstrates the feasibility of using psychrophiles in the development of low-temperature AD systems for biogas production in cold areas of the planet [167].

4. Conclusions

The new strategies tested to improve the AD of lignocellulosic-based materials have provided interesting and viable solutions to tackle the inherent disadvantages of the process itself. The incorporation of pre-treatment technologies such as steam explosion has been found to improve the biodegradability of lignocellulosic biomass, but it requires a detoxification post-pretreatment due to the formation of harmful compounds for digestion, including phenols, furans, and acetic acid. This inconvenience can be solved through the use of ozonolysis or green solvents such as methanol or ethanol, capable of partially solubilizing lignocellulose. Other environmentally friendly solvents such as DESs may also be useful in reducing the recalcitrance of lignocellulosic biomaterials, without the drawbacks of the high viscosity of liquid ions and their high cost. The use of each methodology must be analyzed in detail, balancing its pros and cons. It is important to note that while steam explosion technology is moderately established, others, such as organosolv pre-treatment and DESs are still poorly investigated and understood technologies. Similarly, the study of the efficiency of modern technologies aimed at improving the AD of previously pre-treated biomaterials is showing interesting results. Many of these technologies are focused on increasing microbial activity, significantly enhancing methanogenesis. On the contrary, the alteration of the molecular structure of the plant cell wall by genetic engineering is another approach that, although radically different, might be potentially applicable and provide a less recalcitrant biomass and more easily attackable by microbial enzymes, maintaining the plant cell viability.

Definitely, the recent advances in the AD process of lignocellulosic materials from agri-food waste are providing hopeful results, leading to the gradual but incessant implementation of a circular economy based on the use of plant residues, which are generated in huge amounts during activities related to agriculture and food.

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