

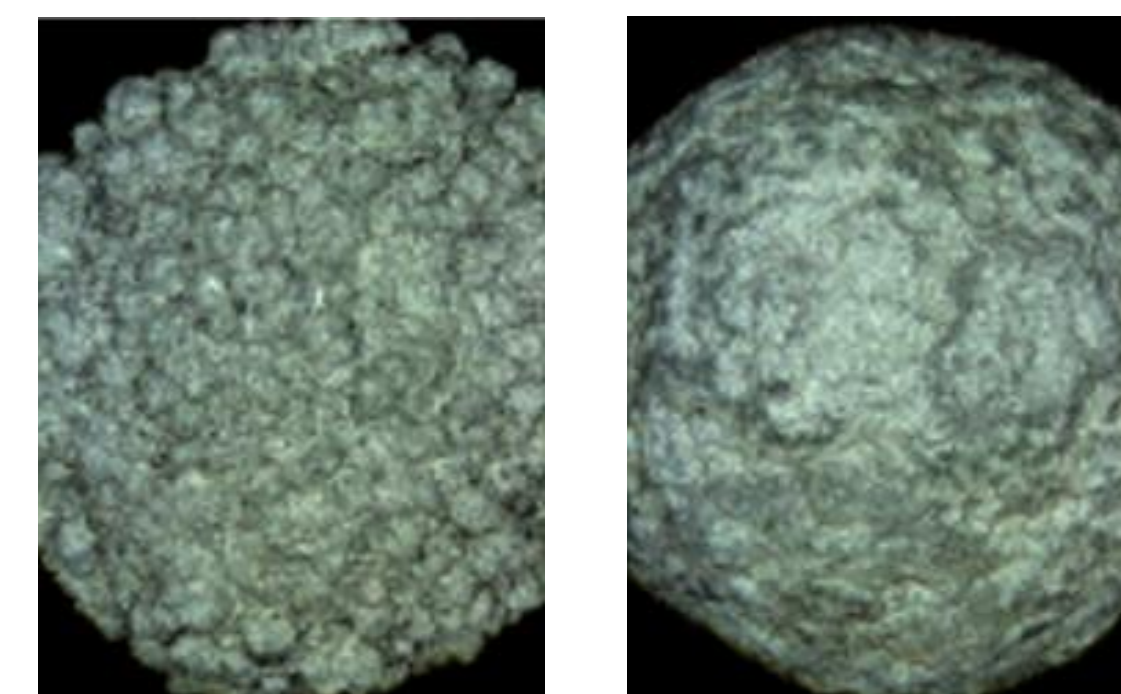
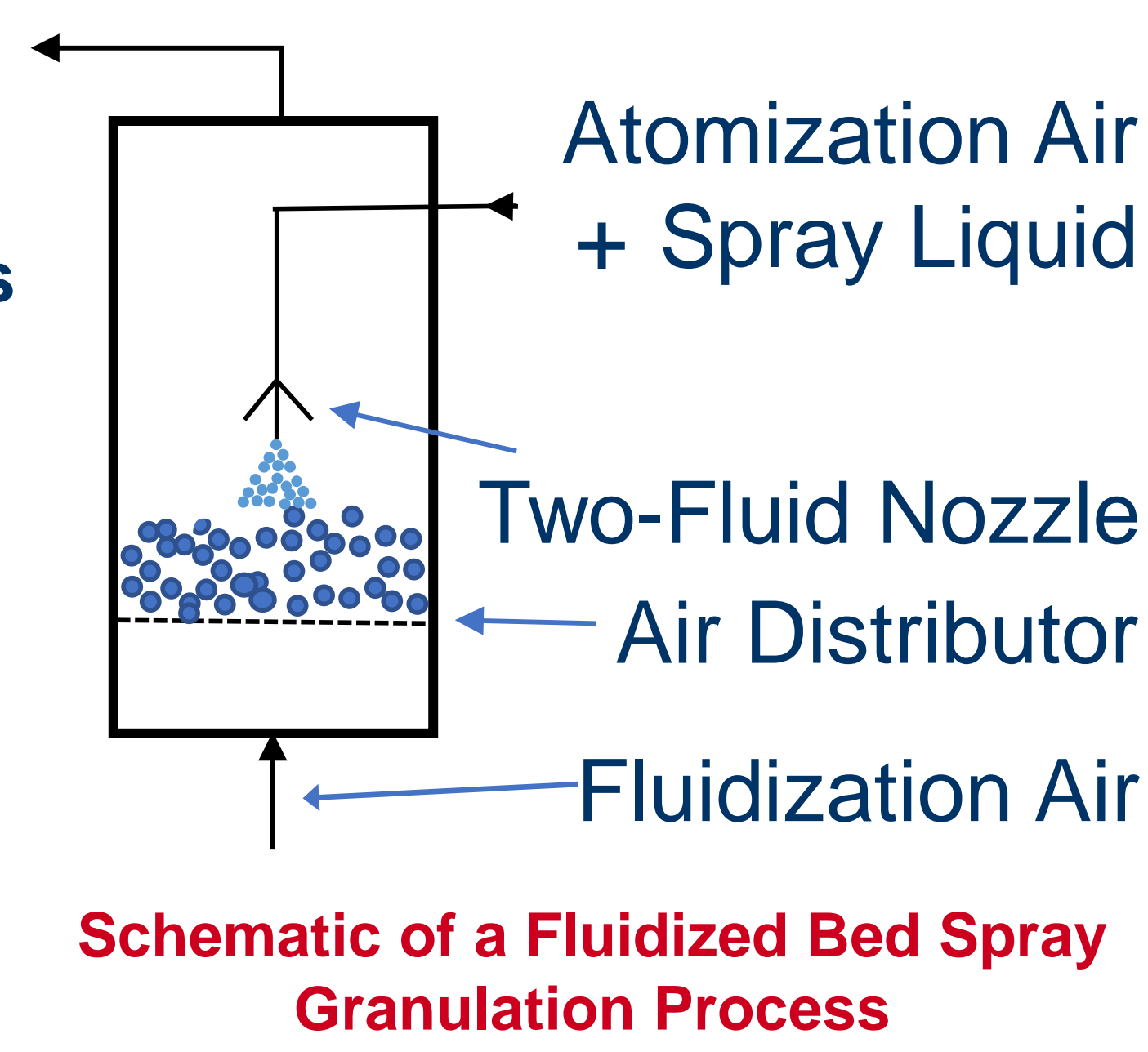
Predicting Product Properties of Fluidized Bed Spray Granulation using CFD-DEM Simulations

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Introduction

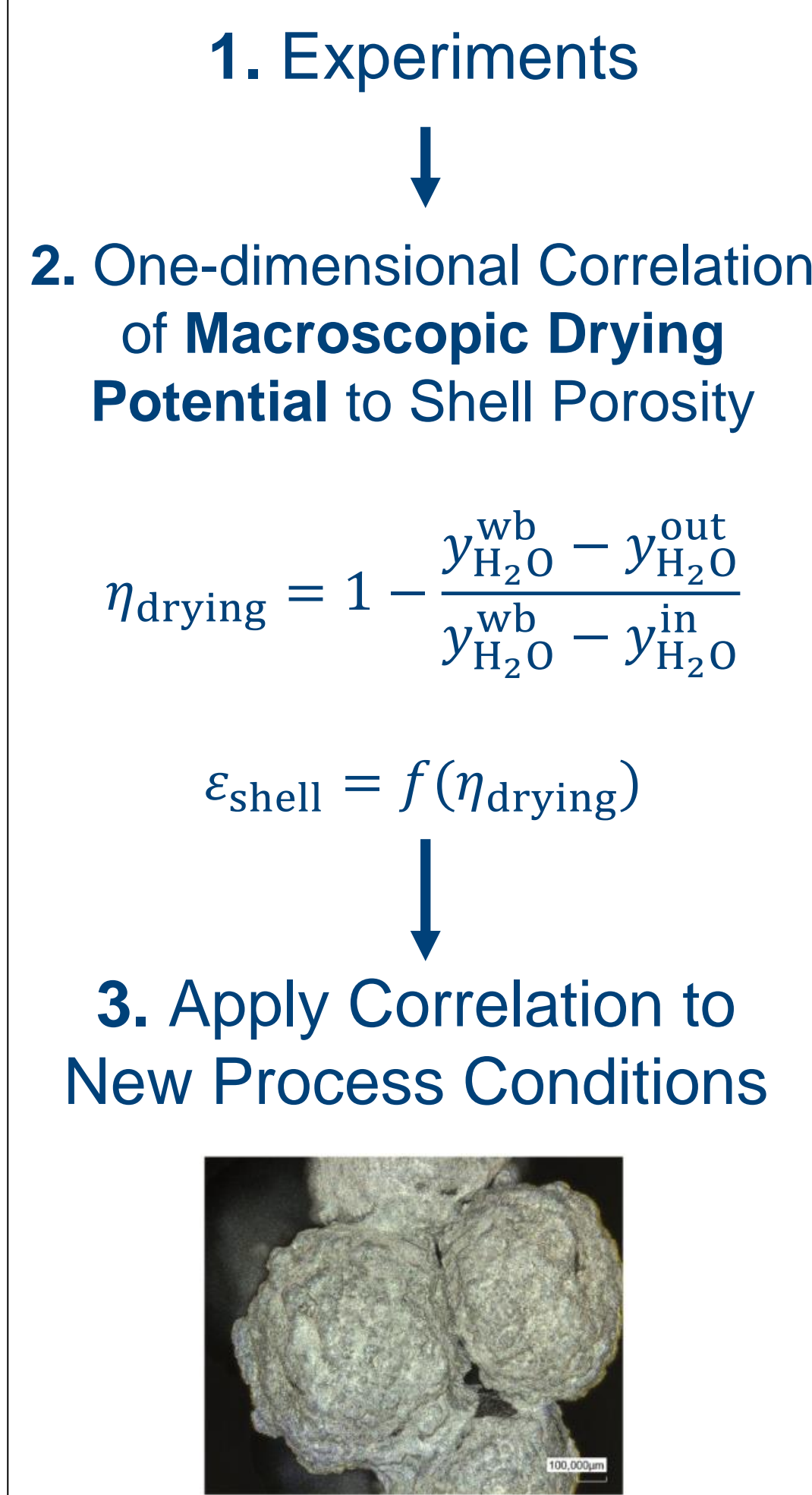
- Fluidized beds are excellent apparatuses for the formation of **tailor-made particles**
- Granulation**: growing particles by spraying coating with solids-containing liquid
- Microprocesses** in droplets and on surface liquid determine **structure** of particle and therefore its properties
- CFD-DEM simulations** provide detailed insight into hydrodynamic behavior of fluidized beds
 - Evaporation of surface liquid, droplet motion and deposition can be tracked for every particle
 - Track **fate of single particle**
 - Track properties of droplets and impact parameters
- Goal**: Predict particle structure from simulations directly



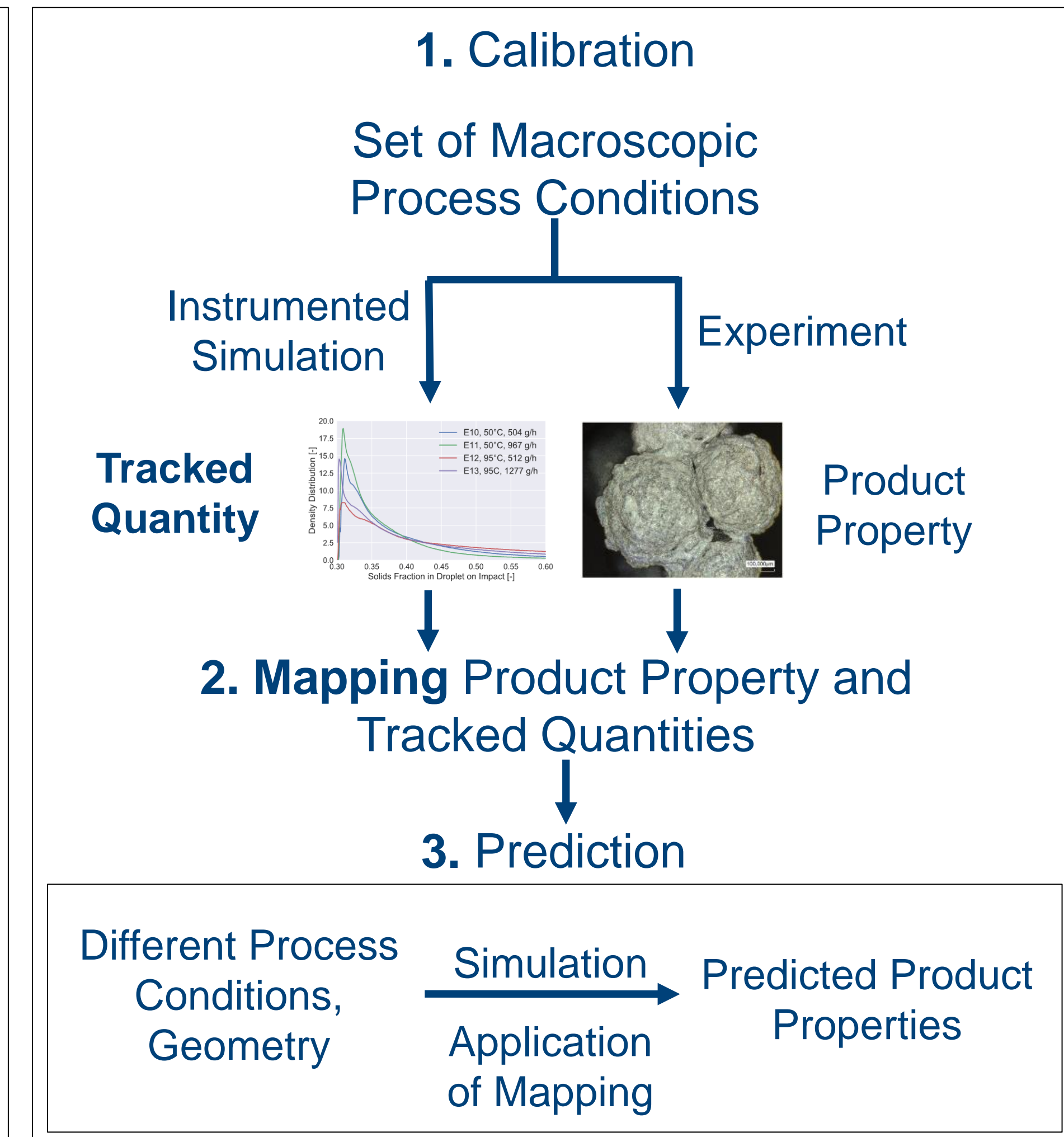
Example Granulation Products exhibiting Different Surface Structures

Workflow for Predicting Product Properties

Prior State of the Art [4,5]



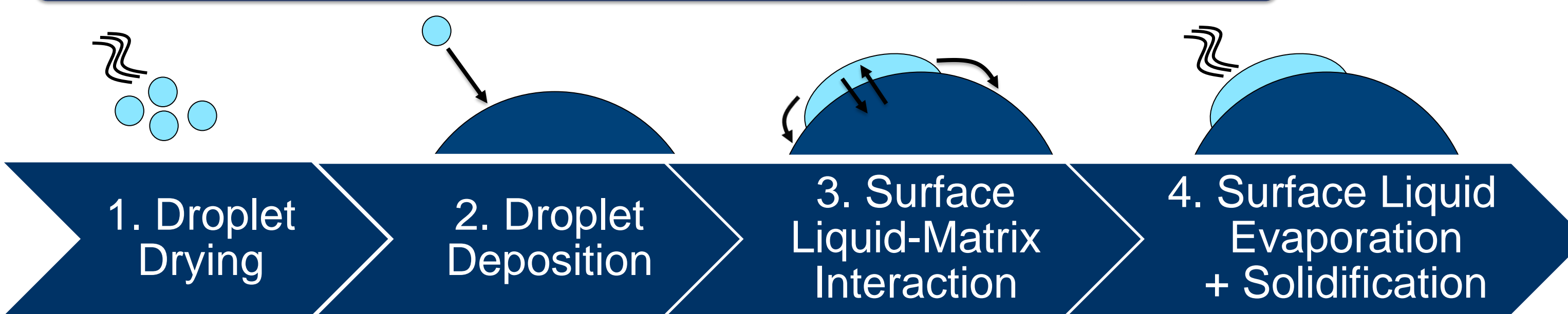
Our Approach



Our approach uses an indirect approach in relating product properties to quantifiers of the microprocesses to their resulting surface structures and thus particle properties. This allows for

- ✓ Prediction of Granulator Geometry Influence
- ✓ Prediction of Scale-Up Effects (incl. dissimilar proportions)
- ✓ Diagnostics of Sub-Par Product Quality compared to the state of the art.

Microprocesses in Layering Spray Granulation



- Droplet drying determines **viscosity at impact**
 - Dependent on droplet size, temperature, humidity, rel. velocity
- High viscosities (= concentrations) at impact correlate negatively with dense layering (= high roughness)
- Surface liquid interacts with surface matrix^[1]
 - Spreading** [2]

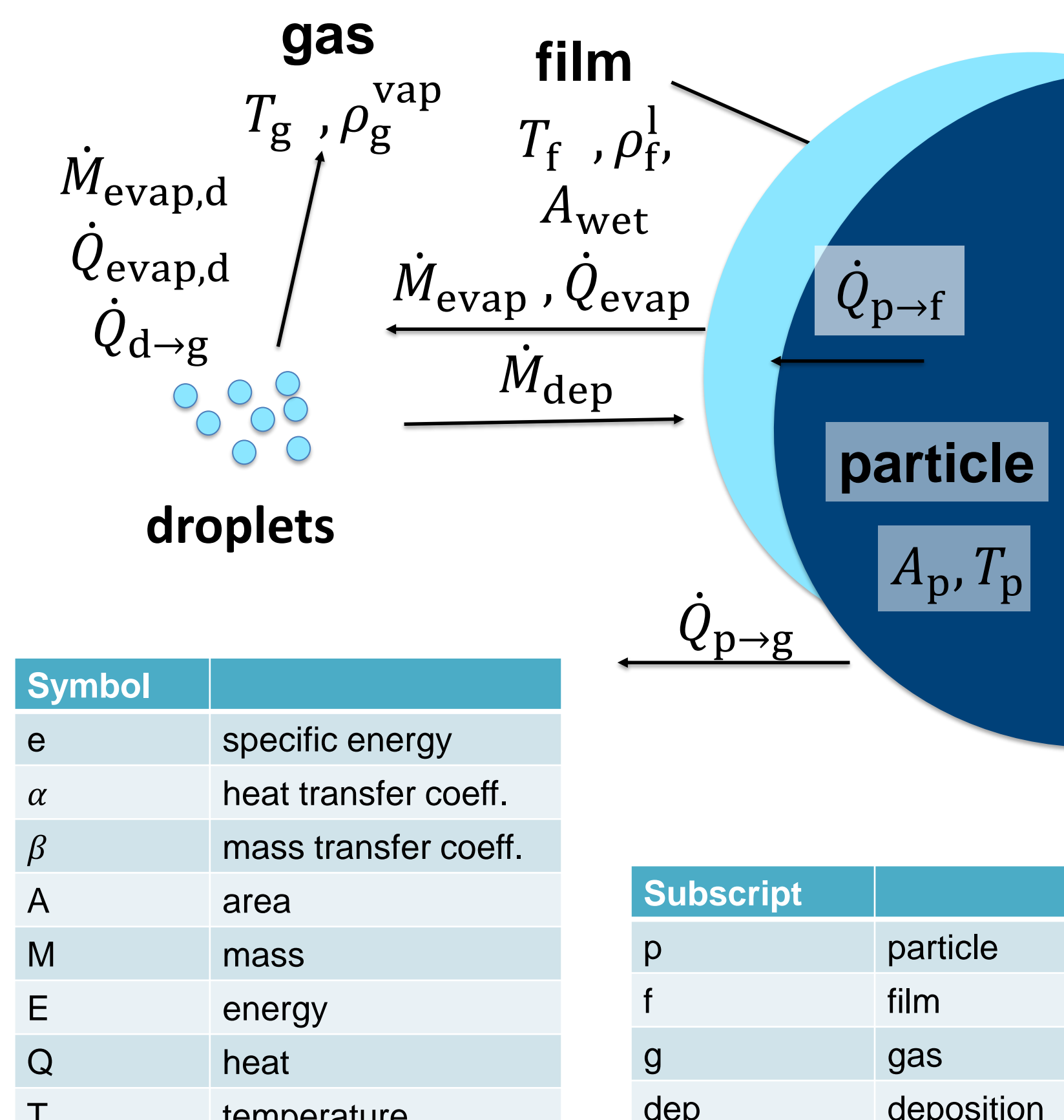
$$R(t) = \left(\frac{24V_{\text{drop}}\sigma(\cos(\theta_0) - \cos(\theta_\infty))}{\pi\eta} \right) t^{1/4}$$
 - Dissolution** [3]

$$\dot{m}_{\text{diss}} = \frac{DA_{\text{layer}}}{h_{\text{layer}}} (c_{\text{layer}}^{\text{sat}} - c_{\text{layer}})$$
 - Imbibition** into pores
- Long event timescales correlate positively with dense layering (= low roughness)

Tracking of **impacted droplet state** and **timescale of drying** can be used as **target variables/tracked quantities** in lieu of resolving surface processes

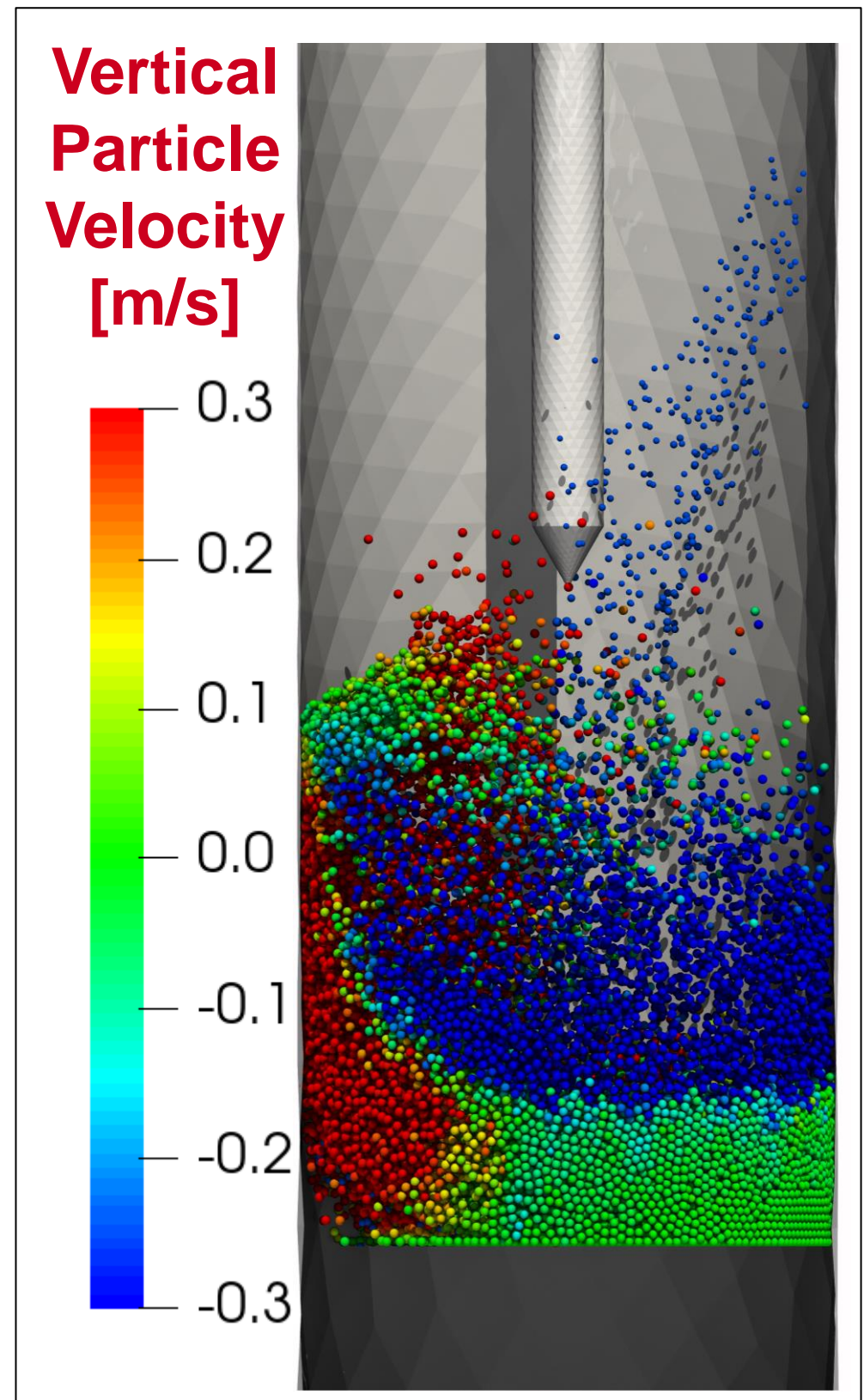
Heat and Mass Transfer Modelling in CFD-DEM

- Balances for film**
 - $\frac{dM_f}{dt} = +\dot{M}_{\text{dep}} - \dot{M}_{\text{evap}}$
 - $\frac{dE_f}{dt} = +\dot{Q}_{\text{dep}} - \dot{Q}_{\text{evap}} - \dot{Q}_{f \rightarrow p} - \dot{Q}_{f \rightarrow g}$
- Balances for gas**
 - $\frac{dM_g}{dt} = +\dot{M}_{\text{evap}}$
 - $\frac{dE_g}{dt} = +\dot{Q}_{\text{evap}} + \dot{Q}_{f \rightarrow g} + \dot{Q}_{p \rightarrow g}$
- Balances for particle**
 - $\frac{dE_p}{dt} = +\dot{Q}_{f \rightarrow p} + \dot{Q}_{p \rightarrow g}$
- Closures**
 - $\dot{M}_{\text{evap}} = \beta A_f (\rho_f^*(T_g, \rho_g) - \rho_g)$
 - $\dot{Q}_{\text{evap}} = \dot{M}_{\text{evap}} \Delta h_{\text{evap}}$
 - $\dot{Q}_{f \rightarrow g} = \alpha_g A_f (T_f - T_g)$
 - $\dot{Q}_{f \rightarrow p} = \alpha_{fp} A_f (T_f - T_g)$
 - $\dot{Q}_{p \rightarrow g} = \alpha_g (A_p - A_{\text{wet}}) (T_p - T_g)$

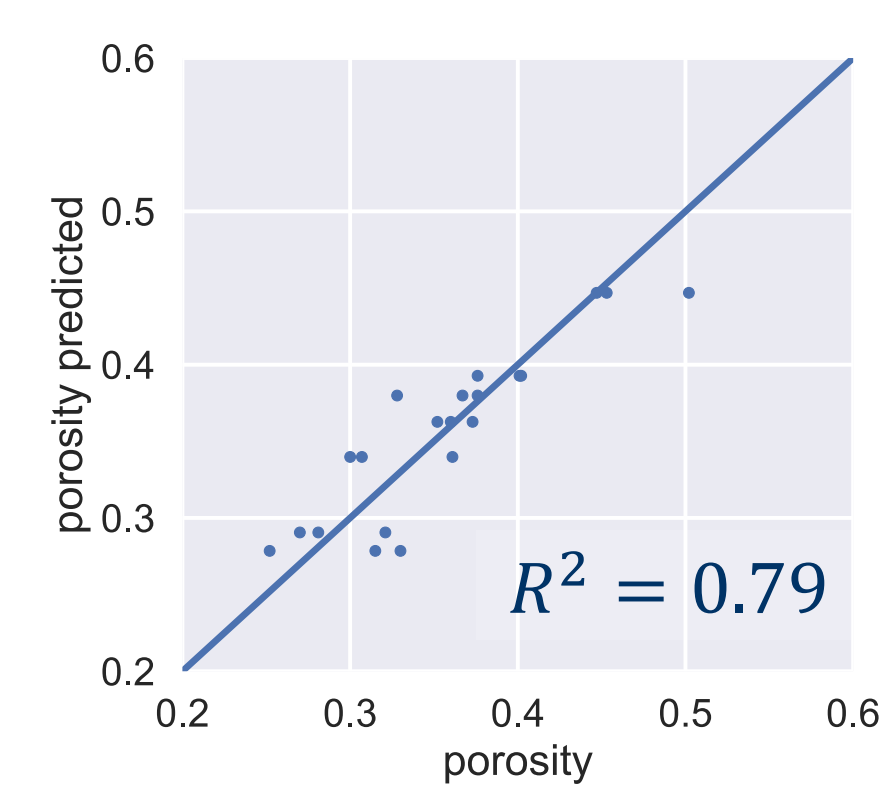


Application: Spray Granulation Case

- Reference experimental case [4] reproduced in simulations
 - Lab-scale (ø 150 mm) top-spray fluidized bed
 - Injection of limestone suspension onto glass particles (d = 650 μm)
 - CT measurement of particle shell porosity
 - Varied spray rate, air temperature $T_{\text{air,in}}$, suspension concentration $x_{\text{susp,in}}$, atomization pressure p_{noz}
- Tracked particle liquid layer **evaporation time** $t_{\text{evap},50}$ and **suspension concentration** x_{susp} in droplets

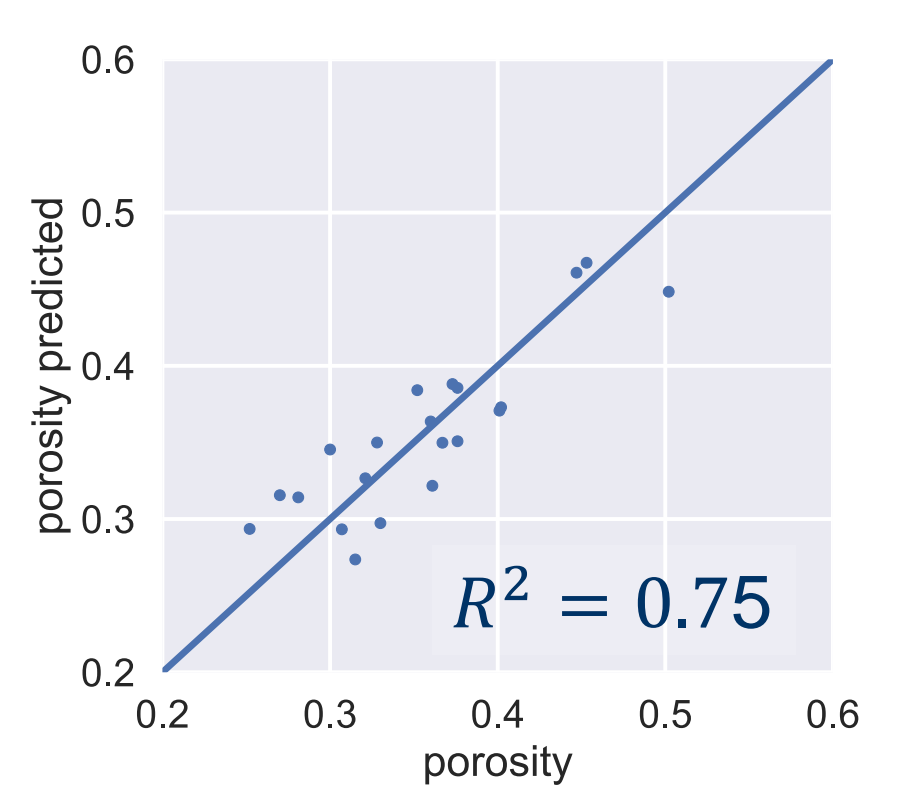


Mapping using Macroscopic Quantities



$$\epsilon_{\text{shell}} = \begin{pmatrix} 1.1E-3 \\ 7.3E-1 \\ -6.0E-3 \end{pmatrix} \cdot \begin{pmatrix} T_{\text{air,in}} \\ x_{\text{susp,in}} \\ p_{\text{noz}} \end{pmatrix} + 0.24$$

Mapping using Micro-Scale Quantities



$$\epsilon_{\text{shell}} = \begin{pmatrix} -8.3E-3 \\ -2.3E-1 \\ 6.8E-1 \end{pmatrix} \cdot \begin{pmatrix} t_{\text{evap},50} \\ t_{\text{evap,skew}} \\ x_{\text{susp},50} \end{pmatrix} + 0.68$$

Microscopic tracked quantities predict the product quality with same confidence as macro-scale parameters (process conditions).

References

- Heine et al.: *Droplet deposition on amorphous particles in a fluidized bed spray agglomeration process*, Granulation Workshop, Lausanne, (2013)
- Ogarev et al.: *Spreading of Polydimethylsiloxane Drops on Solid Horizontal Surfaces*, The Journal of Adhesion, (1974).
- Noyes and Whitney: *The rate of solution of solid substances in their own solutions*, Journal of the American Chemical Society, (1897).
- Schmidt et al.: *Shell porosity in spray fluidized bed coating with suspensions*, Advanced Powder Technology (2017).
- Rieck et al.: *Influence of drying conditions on layer porosity in fluidized bed spray granulation*, Powder Technology (2015).

Next Steps

- Apply method
- Compare granulators with different geometries
- Perform **product-driven, simulation-aided scale-up**
- Develop **resolved pore-scale simulations** of drying to close tracked quantity-surface structure gap

